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MHD thermogravitational convection and thermal radiation of a micropolar nanoliquid in a porous chamber

Mohsen Izadi^a, Mikhail A. Sheremet^{b,*}, S.A.M. Mehryan^c, I. Pop^d, Hakan F. Öztop^{e,f}, Nidal Abu-Hamdeh^f

^a Mechanical Engineering Department, Faculty of Engineering, Lorestan University, Khorramabad, Iran

^b Laboratory on Convective Heat and Mass Transfer, Tomsk State University, 634050 Tomsk, Russia

^c Young Researchers and Elite Club, Yasooj Branch, Islamic Azad University, Yasooj, Iran

^d Department of Mathematics, Babeş-Bolyai University, 400084 Cluj-Napoca, Romania

^e Department of Mechanical Engineering, Technology Faculty, Firat University, Elazig, Turkey

^f Department of Mechanical Engineering, King Abdulaziz University, Jeddah, Saudi Arabia

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ABSTRACT

This work studies the thermogravitational transmission and thermal radiation of micropolar nanoliquid within a porous chamber in the presence of the uniform magnetic influence. The model includes the single-phase nanofluid approach, local thermal equilibrium approximation and Darcy law for the processes within the porous structure. The Galerkin finite element method with the structured non-uniform mesh is used to calculate the formulated equations. The key characteristics are the Darcy-Rayleigh number $Ra = 10\text{--}1000$, Darcy number $Da = 10^{-5}\text{--}10^{-1}$, porosity $\epsilon = 0.1\text{--}0.9$, nanoparticles concentration $\varphi = 0\text{--}0.04$, radiation parameter $R_d = 0\text{--}2$, vortex viscosity characteristic $\Delta = 0\text{--}2$, and Hartmann number $Ha = 0\text{--}50$. It has been ascertained the energy transport intensification with thermal radiation parameter, Darcy-Rayleigh number, porosity and nanoparticles concentration. Also, the results indicate that the average Nusselt number reduces with an increment of the Hartmann number for high values of the Rayleigh number, while for low magnitudes of the Rayleigh number a weak change of the average Nusselt number can be found.

1. Introduction

The convective heat transfer of micropolar fluids is an important topic due to many various applications in description of the flow of slurries, liquid crystals, blood, some polymeric fluids and composite materials [1,2]. The theory of micropolar fluid has been described in detail by Eringen

[3–5]. Nowadays, many different fundamental investigations have been performed for study of convective motion and energy transport in micropolar liquids [6–8]. Thus, Javed and Siddiqui [6] have studied numerically mixed convective circulation and thermal transmission in a chamber with moving border filled with micropolar fluid in the presence of bottom heating and uniform horizontal magnetic influence. It has been found that Hartmann and Reynolds numbers reduce the strength of circulation and isolines of microrotations. Ahmed and Nadeem [7] have investigated numerically MHD micropolar blood circulation in a vertical artery with six various types of stenosis. They have found that the resistance impedance is maximum for the bell-shaped

stenosis and minimum for the trapezoidal one. Sheremet et al. [8] have studied unsteady thermogravitational energy transport of micropolar liquid in an irregular triangular chamber by the finite difference method and non-primitive variables. They have shown the thermal transmission intensity diminution and micropolar liquid circulation suppression with the vortex viscosity parameter. Muthamilselvan et al. [9] have examined numerically thermogravitational convection of micropolar liquid in a cavity with hot thin sheet. The presence of vortex viscosity characteristic suppresses the liquid velocity and hence the thermal transmission intensity. In another paper Muthamilselvan et al. [10] have conducted a numerical study of double-diffusive thermogravitational energy transport of micropolar liquid in a chamber with a heated thin sheet under the Soret and Dufour effects. They have shown the thermal and solute transport enhancement with characteristics of Soret and Dufour. Natural convective boundary-layer circulation combined with thermal radiation of a micropolar liquid close to a vertical plate in the presence of periodic magnetic impact has been analyzed by Siddiqa et al. [11]. Employing the similarity technique, the control

* Corresponding author.

E-mail address: Michael-sher@yandex.ru (M.A. Sheremet).

Nomenclature		Greek symbols
B	magnetic field ($\text{kg}\cdot\text{s}^{-2}\cdot\text{A}^{-1}$)	α thermal diffusivity ($\text{m}^2\cdot\text{s}^{-1}$)
C_p	specific heat ($\text{J}\cdot\text{kg}^{-1}\cdot\text{K}^{-1}$)	β thermal expansion coefficient (K^{-1})
g	gravitational acceleration ($\text{m}\cdot\text{s}^{-2}$)	Δ vortex to molecular viscosity ratio (-)
H	cavity size (m)	ε porosity (-)
Ha	Hartmann number (-)	κ vortex viscosity ($\text{kg}\cdot\text{m}^{-1}\cdot\text{s}^{-1}$)
I	intensity of a current (A)	μ dynamic viscosity ($\text{kg}\cdot\text{m}^{-1}\cdot\text{s}^{-1}$)
j	the micro-inertia density (m^2)	ν kinematic viscosity ($\text{m}^2\cdot\text{s}^{-1}$)
K	permeability of porous medium (m^2)	ρ density ($\text{kg}\cdot\text{m}^{-3}$)
k	thermal conductivity ($\text{W}\cdot\text{m}^{-1}\cdot\text{K}^{-1}$)	σ electrical conductivity ($\text{A}^2\cdot\text{s}^3\cdot\text{kg}^{-1}\cdot\text{m}^{-3}$)
\mathbf{N}	non-dimensional microrotation vector (-)	ϕ volume fraction of nanoparticles (-)
N^*	dimensional microrotation vector (s^{-1})	ψ non-dimensional stream function (-)
p	non-dimensional pressure (-)	ψ^* dimensional stream function ($\text{m}^2\cdot\text{s}^{-1}$)
P^*	dimensional pressure (Pa)	
Pr	Prandtl number (-)	
Ra	thermal Rayleigh number (-)	
T	non-dimensional temperature (-)	
T^*	dimensional temperature (K)	
u, v	non-dimensional components of velocity in x and y directions, respectively (-)	
u^*, v^*	dimensional components of velocity in x^* and y^* directions, respectively ($\text{m}\cdot\text{s}^{-1}$)	
V	non-dimensional velocity vector (-)	
V^*	dimensional velocity vector ($\text{m}\cdot\text{s}^{-1}$)	
x, y	non-dimensional Cartesian coordinates (-)	
x^*, y^*	dimensional Cartesian coordinates (m)	

equations formulated in the form of ordinary differential equations have been calculated by the Keller-box scheme. The skin friction parameter reduces essentially by rising the micro-inertia density and magnetic interaction characteristics, while the opposite nature can be found when the micropolar parameter and thermal radiation parameter are amplified.

Nowadays, solution of different engineering problems demands the heat transfer enhancement. Such heat transfer intensification can be obtained not only by using the additional heat transfer surfaces but also using the nanofluids. In 1995, the term "nanofluid" has been introduced by Choi [12] to describe dilute suspensions formed by nanoparticles less than 100 nm in diameter created early by Masuda et al. [13]. Therefore, a lot of fundamental works deals with an analysis of energy transport in nanoliquids systems [14–46]. Some papers deal with micropolar nanofluids to demonstrate the microrotation and local behavior of the nanofluid units [47,48]. Thus, Hussanan et al. [49] have studied analytically the time-dependent natural convective circulation of five various kinds of oxide nano-sized particles in a micropolar nanoliquid over a vertical plate. They have shown the effects of different nanoparticles material on the heat transfer enhancement. Taking into account the two-phase nanofluid model proposed by Buongiorno [50], Hayat et al. [51] have described the Brownian circulation and thermophoresis effects on micropolar nanoliquid motion. Stretching sheet with linear velocity defines the nanofluid motion under the influence of the radiation and Newtonian heating. It has been shown that the energy and mass transport intensities are amplified for high magnitudes of the radiation and Brownian diffusion characteristics. In addition, heat transfer through porous media has been the subject of many researches [52–62]. Hashemi et al. [63] have investigated computationally thermogravitational thermal transmission in a copper-water micropolar nanofluid porous chamber in the presence of the internal heat generation. It has been pictured that a raise of the Darcy parameter reflects a weak decrease in the intensity of micropolar nanofluid circulation and micro-rotation of particles, while an increment of the vortex viscosity characteristic results in a diminution of the power of particles micro-rotation. Conjugate thermogravitational convection of micropolar

nanoliquid in a porous chamber on the basis of the local thermal non-equilibrium approach has been examined computationally by Mehryan et al. [47]. It has been ascertained that Nu depends on the vortex viscosity for high Ra and it does not depend on this parameter for low Ra . Bourantas and Loukopoulos [48] have analyzed theoretically the free convective energy transport of micropolar nanofluids inside a square enclosure. Using the experimental data for thermophysical properties the authors have discovered some discrepancies between Nu in the case of different experimental correlations. Mixed convective circulation in a water-based micropolar nanoliquid cavity with moving border under the effect of local heater with constant heat flux has been studied numerically by Ahmed et al. [64]. It has been revealed that Nu at the heater reduces as the heater size rises while it enhances when the nanoparticles concentration augments.

Taking into account the previously studied publications and to the authors' best knowledge, there have been no researches of free convective circulation and energy transport of micropolar nanofluid in a porous enclosure with an internal elliptical heat source. Therefore, the main objective of the present investigation is a numerical study of thermogravitational energy transport of micropolar nanoliquid inside a porous chamber having centrally located heated elliptical cylinder under the impact of uniform magnetic influence and thermal radiation.

2. Mathematical description of the problem

A porous square chamber of H size including an elliptic heater located in the center of the cavity is illustrated in Fig. 1. The domain of interest contains the CuO-H₂O micropolar nanoliquid. A magnetic field determined by B vector with amplitude B_0 and inclination angle γ is affected on the cavity. The third coordinate of the cavity that is perpendicular to the cavity and it is much longer compared with the others. The horizontal boundaries of the cavity are adiabatic, while vertical borders are isothermal with constant temperature T_c^* . The isothermal elliptical heat source has high constant temperature T_h^* . Darcy law is considered to define the macroscopic circulation within the chamber. The changes of the chemico-physical parameters of the

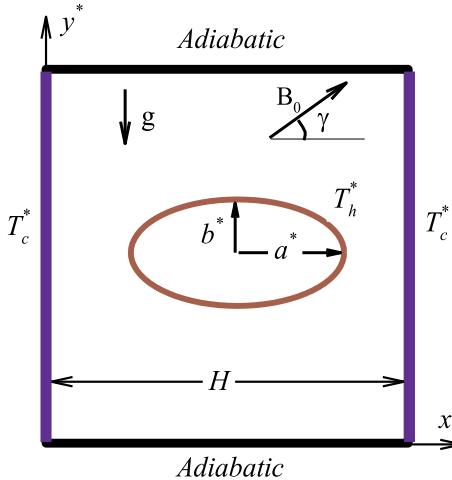


Fig. 1. Domain of interest.

Table 1

The values of coefficients in Eq. (18-d) for CuO-H₂O nanoliquid [73].

The magnitudes of coefficients		CuO-H ₂ O nanofluid
a_1		-26.5933108
a_2		-0.403818333
a_3		-33.3516805
a_4		-1.915825591
a_5		0.06421858
a_6		48.40336955
a_7		-9.787756683
a_8		190.245610009
a_9		10.9285386565
a_{10}		-0.72009983664

Table 2

Mesh sensitivity analysis.

Elements number	3780	5134	6880	9874	11,440
Nu_{avg}	15.458	15.462	15.461	15.459	15.458
$ \psi _{max}$	3.987	3.985	3.983	3.982	3.982

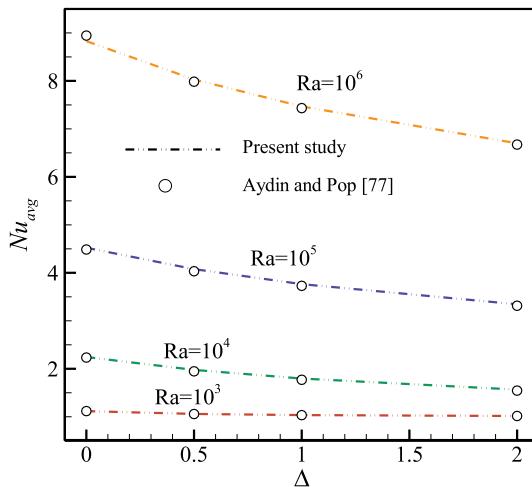


Fig. 2. The average Nusselt number in comparison with numerical results of Aydin and Pop [77].

base liquid and solid particles material are supposed to be negligible except for the density, where the Boussinesq approximation is valid. Local thermal equilibrium approach is assumed between the liquid and

solid structures of the system. The solid particles and base liquid are considered to be equilibrated in the case of velocity and temperature fields. The micro-rotations for micropolar liquid are modeled by including the angular momentum vector to the Navier-Stokes equations considering the volumetric forces appearing due to rotations at micro-level [6,8,47]. Additionally, for the description of the thermal radiation effect the Rosseland approximation is used [65].

Taking into account these models, the control equations are formulated in the following form [66,67]:

$$\nabla \cdot \mathbf{V}^* = 0 \quad (1)$$

$$0 = -\nabla^* p^* - \frac{\mu_{nf} + \kappa}{K} \mathbf{V}^* - (\rho\beta)_{nf}(T^* - T_c^*) \mathbf{g} + \kappa \nabla^* \times \mathbf{N}^* + \mathbf{I} \times \mathbf{B} \quad (2)$$

$$\nabla^* \cdot \mathbf{I} = 0 \quad (3)$$

$$\mathbf{I} = \sigma_{nf}(-\nabla^* \Phi + \mathbf{V}^* \times \mathbf{B}) \quad (4)$$

$$\rho_{nf} j(\mathbf{V}^* \cdot \nabla^*) \mathbf{N}^* = \left(\mu_{nf} + \frac{\kappa}{2} \right) j \nabla^{*2} \mathbf{N}^* + \frac{\kappa}{\varepsilon} \nabla^* \times \mathbf{V}^* - 2\kappa \mathbf{N}^* \quad (5)$$

$$(\rho C_p)_{nf}(\mathbf{V}^* \cdot \nabla^* T^*) = k_{m,nf} \nabla^{*2} T^* - \nabla^* \cdot \mathbf{q}_r \quad (6)$$

where \mathbf{q}_r is

$$\mathbf{q}_r = -\frac{4}{3} \frac{\sigma_e}{\beta_R} \nabla^* T^{*4} \text{ and } T^{*4} = 4T_c^{*3} T^* - 3T_c^{*4} \quad (7)$$

In these equations the bold letters are the vector parameters. Also, j is the micro-inertia density and $j = L^2$, $k_{m,nf}$ is the effective thermal conductivity of the porous structure [68]:

$$k_{m,nf} = (1 - \varepsilon)k_s + \varepsilon k_{nf} \quad (8)$$

where k_{nf} and k_s are the thermal conductivity of the micropolar nanoliquid and solid matrix of the porous system, respectively, and ε is the porosity.

Combining Eqs. (3) and (4) taking into account Garandet et al. [69] we have

$$\nabla^{*2} \Phi = 0 \quad (9)$$

Supposing that cavity borders are electrically insulated, Eq. (9) has the following solution

$$\nabla^* \Phi = 0 \quad (10)$$

Excluding the pressure gradient in motion Eq. (2) and introducing new dependent variable, stream function ($u_{nf}^* = \partial \psi^* / \partial y^*$, $v_{nf}^* = -\partial \psi^* / \partial x^*$), two motion equations can be written as expressed below:

$$\begin{aligned} \frac{\mu_{nf} + \kappa}{K} \left(\frac{\partial^2 \psi^*}{\partial x^{*2}} + \frac{\partial^2 \psi^*}{\partial y^{*2}} \right) &= g(\rho\beta)_{nf} \frac{\partial T^*}{\partial x^*} + \kappa \left(\frac{\partial^2 N^*}{\partial x^{*2}} + \frac{\partial^2 N^*}{\partial y^{*2}} \right) \\ &- \sigma_{nf} B_0^2 \left(\frac{\partial^2 \psi^*}{\partial y^{*2}} \sin^2 \gamma + 2 \frac{\partial^2 \psi^*}{\partial x^* \partial y^*} \sin \gamma \cos \gamma + \frac{\partial^2 \psi^*}{\partial x^{*2}} \cos^2 \gamma \right) \end{aligned} \quad (11)$$

For non-dimensionalization, the following non-dimensional variables are employed:

$$x = x^*/H, \quad y = y^*/H, \quad \psi = \psi^*/\alpha_{m,bf}, \quad T_{nf} = (T_{nf}^* - T_c^*)/(T_h^* - T_c^*), \quad N = (L^2/\alpha_{m,bf})N^* \quad (12)$$

Therefore, one can find

$$\begin{aligned} \frac{\partial^2 \psi}{\partial x^2} + \frac{\partial^2 \psi}{\partial y^2} &= -Ra \frac{(\rho\beta)_{nf}}{(\rho\beta)_{bf}} \left(\frac{1}{\mu_r + \Delta} \right) \frac{\partial T}{\partial x} + Da \left(\frac{\Delta}{\mu_r + \Delta} \right) \left(\frac{\partial^2 N}{\partial x^2} + \frac{\partial^2 N}{\partial y^2} \right) \\ &- Ha^2 \left(\frac{\sigma_r}{\mu_r + \Delta} \right) \left(\frac{\partial^2 \psi}{\partial y^2} \sin^2 \gamma + 2 \frac{\partial^2 \psi}{\partial x \partial y} \sin \gamma \cos \gamma + \frac{\partial^2 \psi}{\partial x^2} \cos^2 \gamma \right) \end{aligned} \quad (13)$$

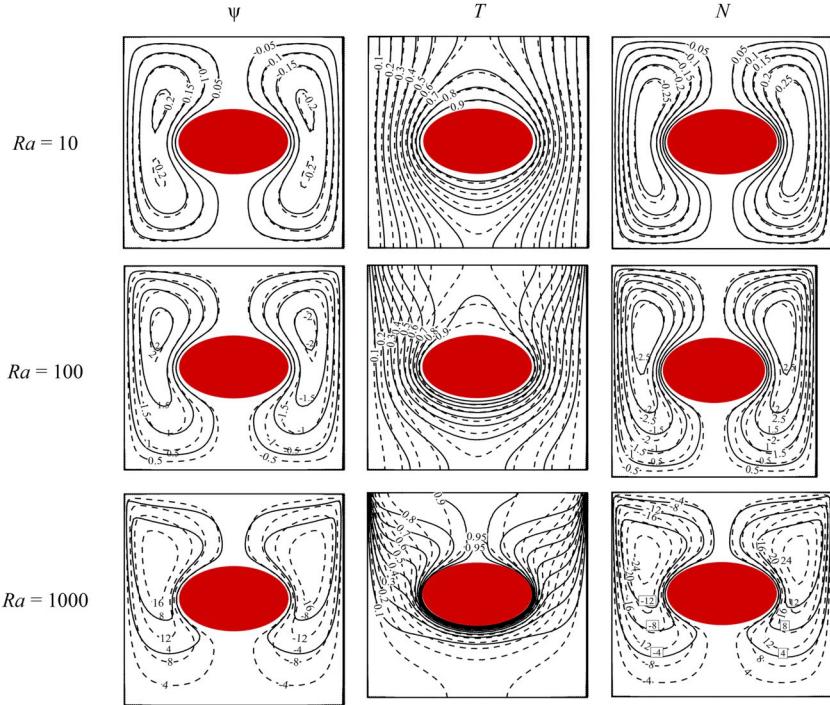


Fig. 3. Streamlines ψ , isotherms T and isolines of microrotation N for different values of the Rayleigh number at $R_d = 0$ (solid lines) and $R_d = 2$ (dashed lines), $\phi = 0.02$, $\epsilon = 0.5$, $Da = 10^{-2}$, $\Delta = 1$, $Ha = 0$.

Table 3

Average Nu magnitudes for porous triangular cavity filled with Cu-H₂O nanoliquid.

Ra	ϕ	Sun and Pop [76]	Sheremet et al. [8]	Present work
500	0	9.66	9.65	9.64
1000	0.1	9.42	9.41	9.42
500	0	13.9	14.05	13.96
1000	0.2	12.85	12.84	12.85

$$\frac{\partial \psi}{\partial y} \frac{\partial N}{\partial x} - \frac{\partial \psi}{\partial x} \frac{\partial N}{\partial y} = Pr \left(\frac{\rho_{bf}}{\rho_{nf}} \right) \left(\mu_r + \frac{\Delta}{2} \right) \left(\frac{\partial^2 N}{\partial x^2} + \frac{\partial^2 N}{\partial y^2} \right) - 2 Pr \Delta \left(\frac{\rho_{bf}}{\rho_{nf}} \right) N + \frac{\Delta Pr}{\epsilon} \left(\frac{\rho_{bf}}{\rho_{nf}} \right) \left(\frac{\partial^2 \psi}{\partial x^2} + \frac{\partial^2 \psi}{\partial y^2} \right) \quad (14)$$

$$\frac{\partial \psi}{\partial y} \frac{\partial T}{\partial x} - \frac{\partial \psi}{\partial x} \frac{\partial T}{\partial y} = \left(\frac{\alpha_{m,nf}}{\alpha_{m,bf}} + \frac{4(\rho C_p)_{bf}}{3(\rho C_p)_{nf}} R_d \right) \left(\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} \right) \quad (15)$$

Here Ra , Da , Pr , Ha , μ_r , σ_r , Δ , R_d , and $\alpha_{m,nf}$ are

$$Ra = \frac{g\beta_{bf}(T_h^* - T_c^*)KH}{\alpha_{bf}\nu_{bf}}, \quad Da = \frac{K}{H^2}, \quad Pr = \frac{\nu_{bf}}{\alpha_{bf}}, \quad Ha = B_0 \sqrt{\frac{\sigma_{bf}K}{\mu_{bf}}}, \quad \mu_r = \frac{\mu_{nf}}{\mu_{bf}}, \quad \sigma_r = \frac{\sigma_{nf}}{\sigma_{bf}}, \quad \Delta = \frac{\kappa}{\mu_{bf}}, \quad R_d = \frac{4\sigma_e T_e^3}{\beta_R k_{m,bf}}, \quad \alpha_{m,nf} = \frac{k_{m,nf}}{(\rho C_p)_{nf}} \quad (16)$$

The boundary conditions are:

$$\begin{aligned} \psi &= 0, \quad N = 0, \quad T = 0 \quad \text{on the left and right vertical walls} \\ \psi &= 0, \quad N = 0, \quad \frac{\partial T}{\partial y} = 0 \quad \text{on the upper and bottom walls} \\ \psi &= C, \quad N = 0, \quad T = 1 \quad \text{on the elliptical heater} \end{aligned} \quad (17)$$

Koo-Kleinstreuer-Li (KKL) approach [70,71] is used to define the nanoliquid chemico-physical parameters:

$$k_{nf} = k_{Static} + k_{Brownian} \quad (18-a)$$

$$\frac{k_{Static}}{k_{bf}} = 1 + \frac{3 \left(\frac{k_{np}}{k_{bf}} - 1 \right) \phi}{\left(\frac{k_{np}}{k_{bf}} + 2 \right) - \left(\frac{k_{np}}{k_{bf}} - 1 \right) \phi} \quad (18-b)$$

$$\frac{k_{Brownian}}{k_{bf}} = 5 \times 10^4 \phi (\rho C_p)_{bf} \left(\frac{\kappa_b T}{\rho_{bf} d_{np}} \right)^{0.5} g'(\phi, T, d_p) \quad (18-c)$$

$$\begin{aligned} g'(\phi, T, d_{np}) &= (a_1 + a_2 \ln(d_{np}) + a_3 \ln(\phi) + a_4 \ln(d_{np}) \ln(\phi) + a_5 \ln(d_{np})^2) \ln(T) \\ &+ (a_6 + a_7 \ln(d_{np}) + a_8 \ln(\phi) + a_9 \ln(d_{np}) \ln(\phi) + a_{10} \ln(d_{np})^2) \end{aligned} \quad (18-d)$$

$$R_f + \frac{d_{np}}{k_{np}} = \frac{d_{np}}{k_{np,eff}}, \quad R_f = 4 \times 10^{-8} m^2 \cdot K/W \quad (18-e)$$

$$\mu_{nf} = \frac{\mu_{bf}}{(1-\phi)^{2.5}} + \frac{k_{Brownian} \mu_{bf}}{k_{bf} Pr} \quad (19)$$

The other thermophysical parameters of the nanoliquid are [72]:

$$\begin{aligned} \rho_{nf} &= (1-\phi)\rho_{bf} + \phi\rho_{np}, \quad \alpha_{nf} = \frac{k_{nf}}{(\rho C_p)_{nf}}, \\ (\rho\beta)_{nf} &= (1-\phi)(\rho\beta)_{bf} + \phi(\rho\beta)_{np}, \\ (\rho C_p)_{nf} &= \phi(\rho C_p)_{np} + (1-\phi)(\rho C_p)_{bf} \end{aligned} \quad (20)$$

Parameters for the additional function g' presented in Eq. (18-d) for the CuO-water nanofluid can be seen in Table 1.

3. Procedure of solution, grid independency test and validation

A numerical technique based on the Galerkin finite element is used for computations. Detailed discussion of the employed computational algorithm is in [74,75]. Initially the grid independence test has been performed for the following parameters $Ra = 10^3$, $\epsilon = 0.5$, $Da = 10^{-2}$,

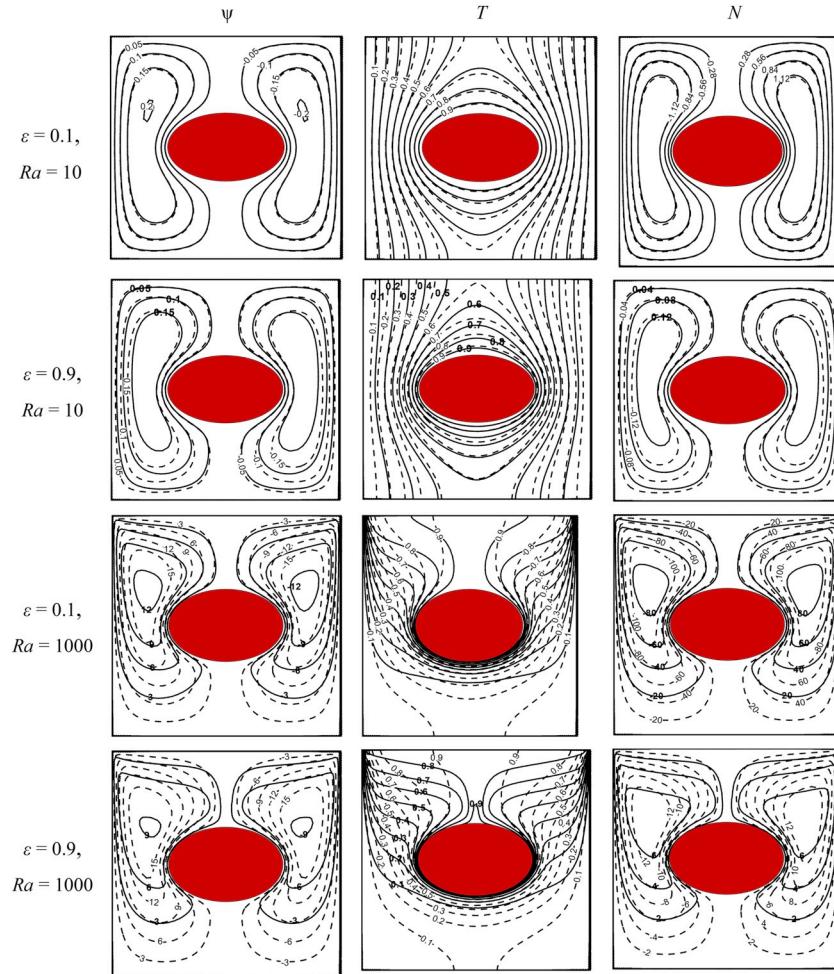


Fig. 4. Streamlines ψ , isotherms T and isolines of microrotation N for various Rayleigh numbers and porosities at $R_d = 0$ (solid lines) and $R_d = 2$ (dashed lines), $\phi = 0.02$, $Da = 10^{-2}$, $\Delta = 1$, $Ha = 0$.

$\Delta = 1$, $R_d = 1$, $Ha = 10$, $\gamma = \pi/2$ and $\phi = 0.04$. The data of this validation, as presented in Table 2, characterize that a mesh of 9874 elements is enough for analysis.

In the case of benchmark analysis several problems from literature [47,76,77] have been studied using the developed numerical technique. A good agreement has been obtained that can be found in Figs. 2, 3 and Table 3.

4. Results and discussion

Analysis of the control characteristics influence (Darcy-Rayleigh number $Ra = 10\text{-}1000$, porosity $\epsilon = 0.1\text{-}0.9$, Darcy number $Da = 10^{-5}\text{-}10^{-1}$, radiation parameter $R_d = 0\text{-}2$, nanoparticles concentration $\phi = 0\text{-}0.04$, vortex viscosity characteristic $\Delta = 0\text{-}2$, Hartmann number $Ha = 0\text{-}50$) on the velocity and temperature fields as well as the rates of thermal transmission has been performed.

Fig. 3 shows the impact of radiation characteristic on isolines of stream function, temperature, and micro-rotations at various Ra . The effect of radiation parameter on these characteristics increases with increasing in Ra . A raise of the Rayleigh number breaks the symmetry between the flow and the horizontal centerline passing through the cavity owing to the domination of convective energy transport over the conductive heat transfer. In general, the flow rate rises for high Ra , considering the radiation parameter. The radiative and molecular diffusions change the patterns of isothermal lines and temperature distribution (see Eq. (15)). On the other hand, the radiative diffusion can reduce the flow viscosity and resistance against fluid movement,

thereby increasing the flow rate. These conditions can result in a greater flow mixture throughout the enclosure and improve the cooling and heat transfer parameters. Finally, the angular momentum affecting the liquid volumes inside the pores of the porous system increases with a raise of the radiation characteristic and flow rate at high Rayleigh numbers, increasing the micro-rotation power.

Fig. 4 demonstrates the influence of radiation number on streamlines, isothermal lines, and isomicro-rotations at different porosities. According to this figure, the influence of this characteristic on the streamlines and micro-rotations increases with increasing in the porosity at low Rayleigh numbers. It seems that a greater volume of fluid is affected by the radiative heat transfer at an increased porosity coefficient. In addition, the resistance against the nanofluid particle movement reduces with reducing the viscosity, resulting in a weak increment of the circulation intensity. Moreover, the angular momentum affecting the liquid volumes increases with a growth of the porosity coefficient under the radiation effects, thereby increasing the micro-rotation power. In contrast, the effect of radiation parameter can be seen at both high and low porosity with increasing in the Rayleigh number and buoyancy forces. According to the first and second rows, an increase in the porosity does not significantly affect the streamlines at low Rayleigh numbers. In contrast, an increase in the porosity (the third and fourth rows) reduces the power of flow lines at high Ra . In addition, the reduction in micro-rotation power is intensified with increasing the porosity. This reduction is owing to a reduction of the angular momentum affecting the liquid volumes with increasing in the size of porous medium's pores. The effect of an increase in the porosity on the

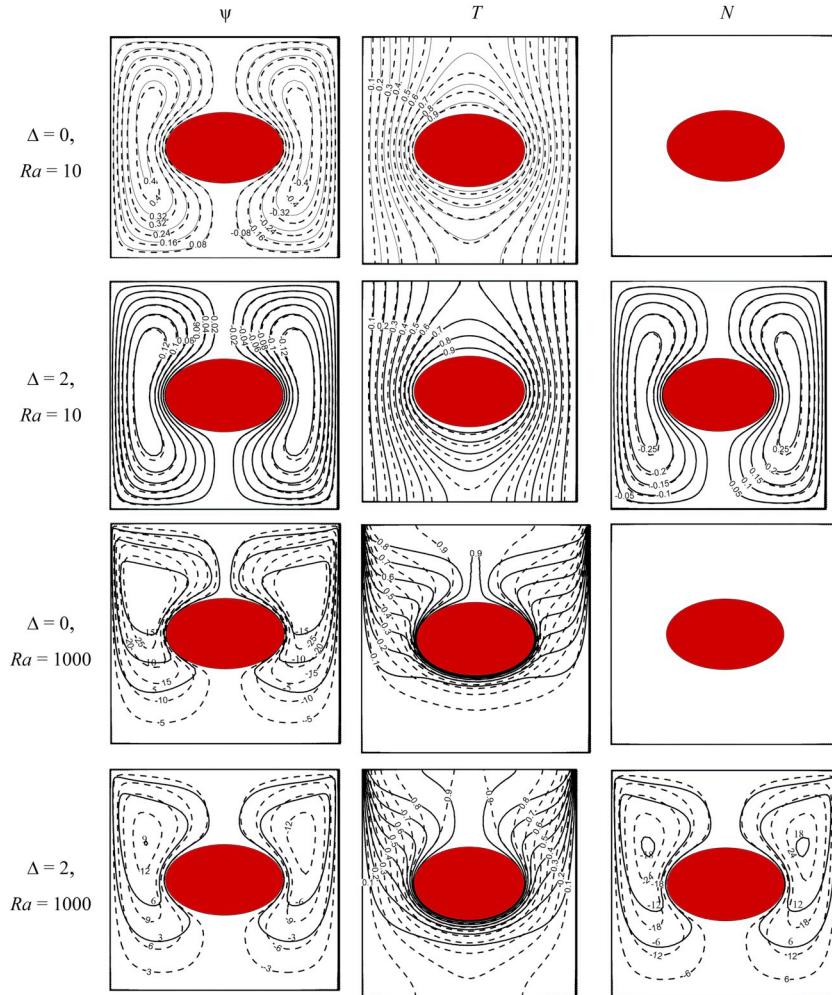


Fig. 5. Streamlines ψ , isotherms T and isolines of microrotation N for various Rayleigh numbers and vortex viscosity at $R_d = 0$ (solid lines) and $R_d = 2$ (dashed lines), $\phi = 0.02$, $\epsilon = 0.5$, $Da = 10^{-2}$, $Ha = 0$.

isothermal lines is reflected as a reduction in the boundary layer thickness, specifically in the region above the elliptical heater, where the greater concentration of the isothermal lines can increase the Nusselt number with increasing the porosity.

Fig. 5 shows the impacts of radiation number and vortex viscosity on isolines of stream function, isotherms and isolines of micro-rotations at different Rayleigh numbers. Application of vortex viscosity, along with molecular viscosity, increases the resistance against fluid particle movement and reduces the flow rate. These conditions apply to both high and low Rayleigh numbers. However, a greater reduction in the flow rate is observed at lower Rayleigh numbers.

This is because the effect of resistance to particle movement is greater at lower buoyancy force. In addition, the influence of radiation characteristic on the isotherms significantly rises with increasing in Ra , resulting in a significant change in temperature distribution.

Fig. 6 demonstrates the impact of Ha and Ra on isolines of stream function, temperature, and micro-rotations. According to this figure, a growth of Ha at both high and low Rayleigh numbers not only reduces the flow rate, but also results in an overall change in the flow pattern. The Lorentz force acts in an opposite direction to the buoyancy forces, reducing the power of streamlines. The effect of radiation parameter is reduced with the application of magnetic field, specifically at high Rayleigh numbers, and the streamlines overlap for different radiation parameters. Also, it can be observed a similar micro-rotation behavior. The angular momentum affecting the liquid volumes, caused by the buoyancy force, reduces with the application of the angular momentum

in an opposite direction, caused by the Lorentz force, resulting in reduced micro-rotation power. The isotherms distortion, caused by an increase in the buoyancy force, significantly rises with increasing in the Rayleigh number from 10 to 10^3 and results in a longitudinal stretch, indicating a growth of the natural convective heat transfer. However, the effect of radiation parameter on the isotherms significantly reduces with increasing in the Lorentz force resistance to the fluid particle movement and decreasing in the flow rate at $Ra = 10^3$ and $Ha = 50$.

Fig. 7 illustrates Nu changes with the radiation parameter and Rayleigh number. According to this figure, the Nusselt number rises with a growth of Ra and radiation parameter. An amplification of Ra increases the circulation intensity and natural convective energy transport. An increase in the radiation parameter (Fig. 3) changes the isothermal lines, resulting in a rise of Nu .

Fig. 8 shows the mean Nu changes with R_d and ϕ at various Ra . According to this figure, although Nu is relatively independent on ϕ at a low Ra ($Ra = 10$), it increases with a growth of ϕ at high Rayleigh number ($Ra = 10^3$). The effect of nanoparticles inclusion to the host liquid amplifies with a growth of the Rayleigh number. In fact, a rise of nano-sized particles concentration results in a slight increase in the thermal diffusion of nanofluid and therefore, increases mean Nusselt number.

Fig. 9 presents the changes of the mean Nu with radiation parameter and porosity at two different Rayleigh numbers. According to this figure, Nu_{avg} raises with increasing in the porosity. The shear stress acting on the nanofluid particles in the cavity reduces with increasing

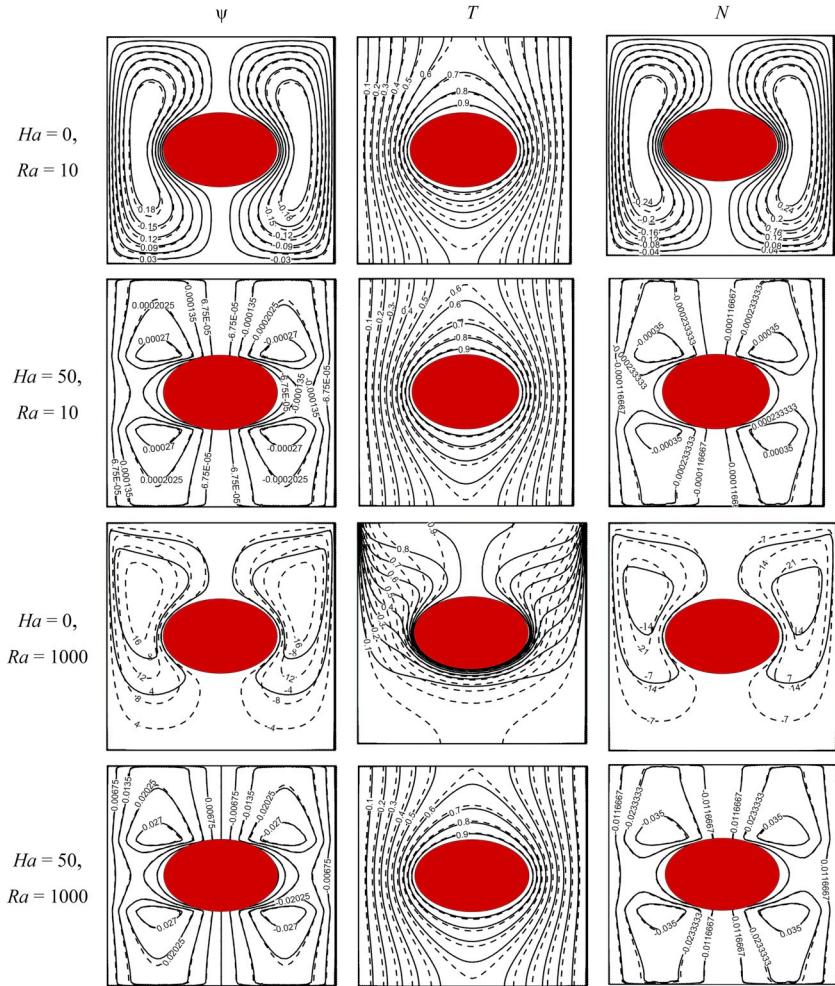


Fig. 6. Streamlines ψ , isotherms T and isolines of microrotation N for various Rayleigh and Hartmann numbers at $R_d = 0$ (solid lines) and $R_d = 2$ (dashed lines) at $\phi = 0.02$, $\epsilon = 0.5$, $Da = 10^{-2}$, $\Delta = 1$.

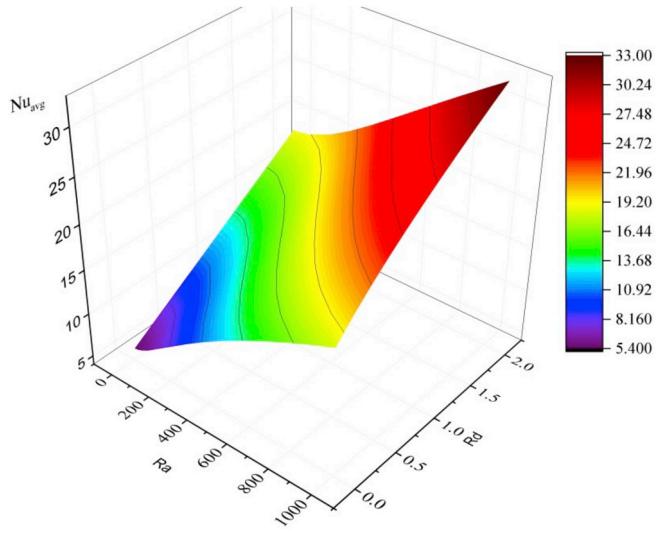


Fig. 7. Changes of Nu_{avg} with radiation characteristic and Rayleigh number.

the porosity and size of the porous medium's pores, reducing the resistance against fluid particle movement. This phenomenon increases the flow power and improves the convective heat transfer.

Fig. 10 indicates the independence of the mean Nusselt number from vortex viscosity at low Ra ($Ra = 10$). In contrast, the mean Nu

reduces with increasing in the vortex viscosity at higher Rayleigh number ($Ra = 10^3$). This behavior suggests that the influence of vortex viscosity on the convective thermal transmission increases with the natural convective heat transfer dominating the conductive energy transport. The motion intensity reduces with increasing the vortex viscosity, weakening its ability in convective energy transport and reducing Nu .

Fig. 11 demonstrates the mean Nusselt number variation by Hartmann number and radiation parameter at two different Rayleigh numbers. According to this figure, although an increase in the Hartmann number, meaning a greater Lorentz force effect on the fluid particles, does not change the mean Nu at low Ra ($Ra = 10$), Ha and the Lorentz force can affect the Nusselt number through increasing the buoyancy at high Rayleigh numbers ($Ra = 10^3$). Under these conditions, Nu_{avg} reduces with an increment of Ha . This effect has a limited amplitude, which continues to approximately $Ha = 10$, after which the mean Nusselt number becomes independent on the Hartmann number again, due to the weakening of the buoyancy force.

5. Conclusion

MHD natural convection and thermal radiation of micropolar nanofluid in a square porous chamber with centered isothermal elliptical heat source have been studied. A complex analysis for liquid circulation and energy transport combined with average Nusselt number has been computationally conducted by the finite element method. The

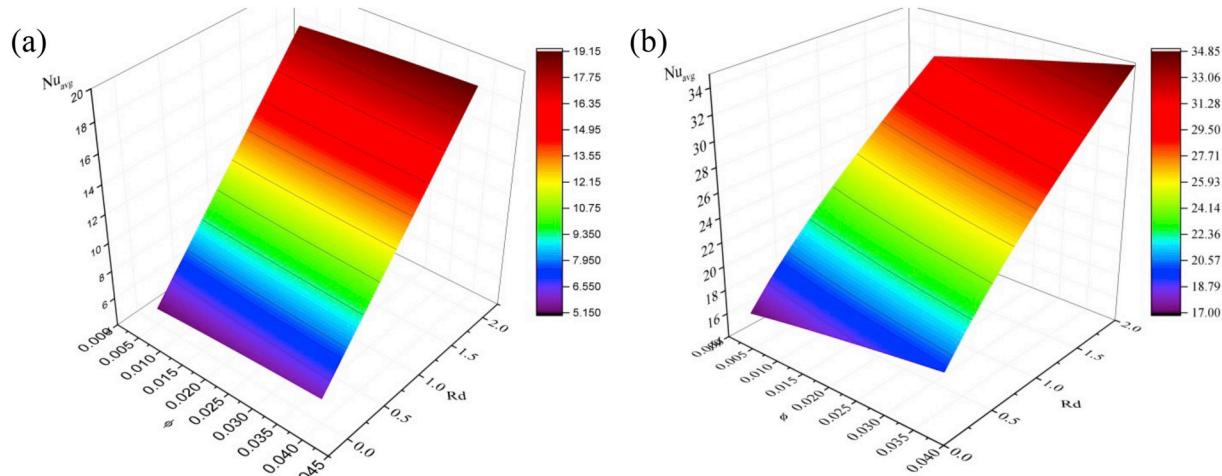


Fig. 8. Surface variation of Nu_{avg} (a) $Ra = 10$ and (b) $Ra = 10^3$ with radiation parameter and volume fraction of nanoparticles.

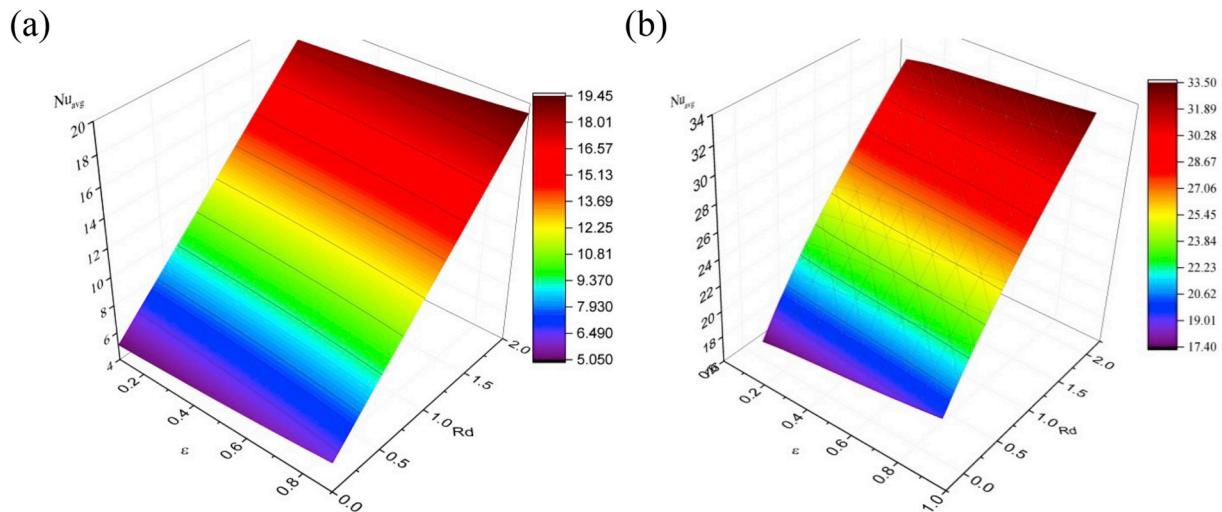


Fig. 9. Surface variation of Nu_{avg} (a) $Ra = 10$ and (b) $Ra = 10^3$ with radiation parameter and porosity coefficient.

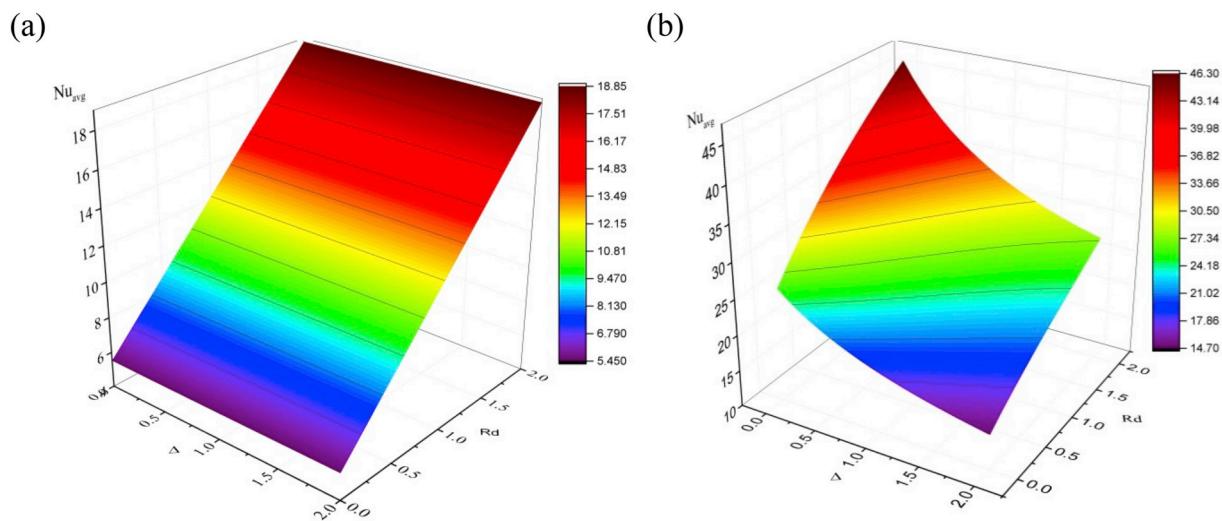


Fig. 10. Surface variation of Nu_{avg} (a) $Ra = 10$ and (b) $Ra = 10^3$ with radiation parameter and vortex viscosity.

governing characteristics for the present study were the Darcy-Rayleigh number $Ra = 10\text{--}1000$, porosity $\varepsilon = 0.1\text{--}0.9$, Darcy number $Da = 10^{-5}\text{--}10^{-1}$, radiation parameter $R_d = 0\text{--}2$, Hartmann number $Ha = 0\text{--}50$, nanoparticles concentration $\phi = 0\text{--}0.04$, and vortex

viscosity characteristic $\Delta = 0\text{--}2$. The streamlines, isotherms and isolines of microrotation combined with the mean Nusselt number for mentioned governing characteristics have been studied. The following results have been revealed:

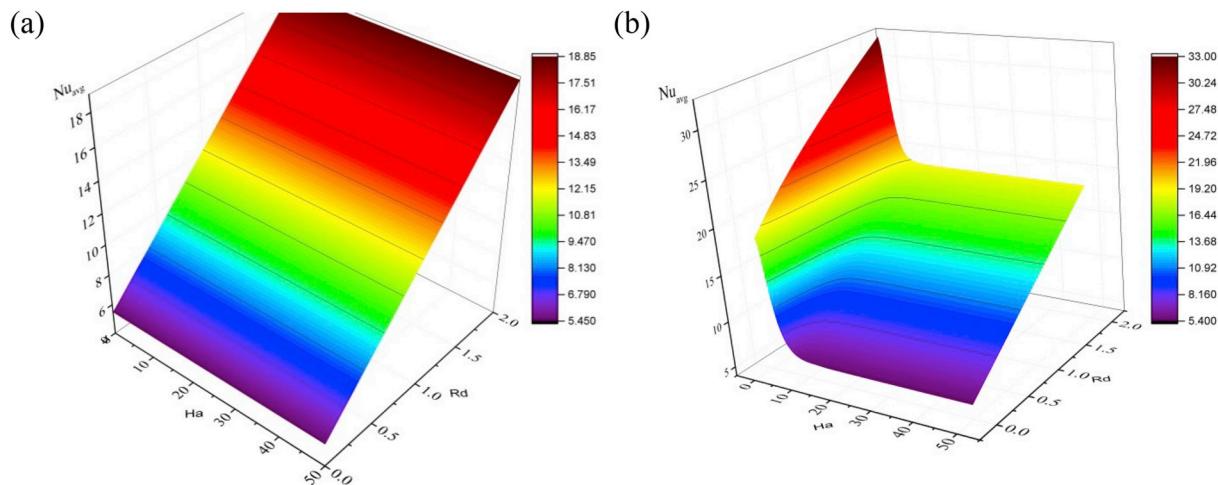


Fig. 11. Surface variation of Nu_{avg} (a) $Ra = 10$ and (b) $Ra = 10^3$ with Hartmann number and radiation parameter.

- A rise of Ra leads to the thermal transmission intensification and nanofluid circulation strengthening.
- High Ra numbers illustrate a drift of convective cells cores in the upper part over the heated element.
- A rise of the thermal radiation parameter illustrates a growth of both Nu_{avg} and nanofluid circulation intensity.
- The effect of porosity is more visible for high Ra and low values of the thermal radiation parameter, namely, a growth of ϵ results in the convective energy transport intensification.
- Increment of ϕ and R_d increases Nu_{avg} , that is more significant for high Ra .
- Average Nusselt number reduces with an increment of Ha for high Ra , while for low Ra a weak change of Nu_{avg} can be found.
- Behavior of microrotation can be described using the streamlines.
- A growth of the vortex viscosity characteristic reflects the thermal transmission suppression and convective motion attenuation inside the cavity.

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