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High-Temperature Abatement of N₂O over FeOx/CeO₂-Al₂O₃ Catalysts: The Effects of Oxygen Mobility

Larisa Pinaeva¹, Igor Prosvirin¹, Yuriy Chesalov¹ and Victor Atuchin^{2,3,4,5,*}

- ¹ Boreskov Institute of Catalysis SB RAS, 5, Lavrentiev ave, Novosibirsk 630090, Russia
- ² Laboratory of Optical Materials and Structures, Institute of Semiconductor Physics, SB RAS, Novosibirsk 630090, Russia
- ³ Research and Development Department, Kemerovo State University, Kemerovo 650000, Russia
- ⁴ Department of Industrial Machinery Design, Novosibirsk State Technical University, Novosibirsk 630073, Russia
- ⁵ R&D Center "Advanced Electronic Technologies", Tomsk State University, Tomsk 634034, Russia
- * Correspondence: atuchin@isp.nsc.ru

Abstract: CeO₂-Al₂O₃ oxides prepared by co-precipitation (Ce+Al) or CeOx precipitation onto Al₂O₃ (Ce/Al) to obtain dispersed CeO₂ and samples with further supported FeOx (2.5–9.9 weight% in terms of Fe) were characterized by XRD, XPS, DDPA and Raman. Fe/Ce/Al samples with lower surface concentrations of Fe³⁺ were substantially more active in N₂O decomposition at 700–900 °C. It was related to higher oxygen mobility, as estimated from ¹⁶O/¹⁸O exchange experiments and provided by preferential exposing of (Fe-)Ce oxides. Stabilization of some Ce as isolated Ce³⁺ in Fe-Ce-Al mixed oxides dominating in the bulk and surface layers of Fe/(Ce + Al) samples retards the steps responsible for fast additional oxygen transfer to the sites of O₂ desorption.

Keywords: N2O decomposition; Fe-Ce-Al mixed oxide; oxygen mobility

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1. Introduction

Nitric acid is a key chemical with annual production at above 65 million tons mainly driven by the fertilizer industry. Nitrous oxide (N₂O) is produced as an unwanted, but inevitable by-product at HNO₃ industrial manufacture by ammonia oxidation. Its emissions by nitric acid plants are growing from 5 to 12 kg N₂O/ton HNO₃ according to the tendency to high-pressure processes [1]. Meanwhile, nitrous oxide is a potent greenhouse gas characterized by about 300 times the Global Warming Potential of CO₂ and contributes to the greenhouse effect and ozone layer depletion. Therefore, 330-780 thousand tons of N₂O annually emitted at HNO₃ production are equivalent to 100-240 million tons/y CO₂e. It can be deleted by placing the catalysts in several points of the ammonia processing flowsheet [2], including that immediately downstream the Pt–Rh gauzes operating at 800–900 °C. A tendency of recent years to increase weight space velocity and reduce the charge of platinum-group metals in the reactor increased the risk of ammonia slipping at gauze ageing or damage. Therefore, efficient conversion of NH₃ to NO + NO₂, while N₂O is low is one of the necessary features for N₂O decomposition catalysts operating in these conditions as well.

Fe-Al-O-based catalytic compositions are efficient both in selective ammonia oxidation to NO and NO₂ [3–5] and in selective N₂O decomposition under the conditions of the nitric acid plant [4–8] without decrease in NOx yield [6,7]. The activity in both reactions was shown to increase by using CeO₂ as the support instead of alumina [4]. It was due to the appearance of the additional pathway of the oxygen supply through oxygen vacancies located in the near subsurface layers of ceria to Fe active sites facilitating the rate-determining step of O₂ desorption. An increase in both ceria and Co(Fe)O_x dispersion could

Catalysts 2022, 12, 938 2 of 16

additionally promote oxygen diffusion to Fe. In the first case it is because both distributions of oxygen vacancies and oxygen storage and release capability of CeO₂ are related to its particle size [9,10]. The positive effect of the dispersion of Co oxide spinel phase [11,12] or FeOx species over ceria and alumina [4,5,8] onto activity in both reactions was already shown and related to enhanced oxygen diffusion through the active component/support interface periphery [4,11,12]. However, for individual CeO₂ all positive effects resulting from fast oxygen transfer are restricted by its low surface area under the reaction conditions [10]. Several methods to stabilize dispersed CeO₂ particles over Al₂O₃ after calcination at above 800°C were reported. They include the sol–gel method using aluminum tri-sec-butoxide and Ce(III) nitrates as precursors [13], impregnation of alumina with an aqueous solution of (NH₄)₂[Ce(NO₃)₆] [14] or stabilization of a complex of the CeO₂ precursor in a homogeneous polymeric matrix (Pechini route) followed by supporting onto alumina [15,16].

In the current study, we used CeO₂ precipitation onto Al₂O₃ or CeO₂ and Al₂O₃ coprecipitation methods to increase CeO₂ dispersion in the final supports compared with individual CeO₂. The reasons for the principally different activity of FeOx/CeO₂-Al₂O₃ samples prepared using these supports have been elucidated.

2. Results and Discussion

2.1. Phase Composition (XRD)

XRD patterns of Ce/Al and (Ce + Al) samples revealed a mixture of CeO₂, θ -Al₂O₃ and γ -Al₂O₃, phases (Figure S1 in Supporting Information). Lattice parameters of CeO₂ in both samples were exactly the same (Table 1) and practically coincided with those for pure CeO₂ calcined at 900 °C (a = b = c = 5.412 Å), while the values of coherent scattering area dxrD calculated by the Scherrer equation were lower (40 and 11 nm for Ce/Al and (Ce + Al), respectively, compared with 68 nm for pure CeO₂ [4]). Lattice parameters of γ (+ θ)-Al₂O₃ phases cannot be calculated correctly because of low intensity and substantial broadening of corresponding overlapping signals. Therefore, some penetration of Ce ions into their lattices cannot be excluded. At the same time, higher dispersion of alumina species in the (Ce + Al) sample follows from larger widths of the peaks at 45.5° and 67.0° (Figure S1).

Table 1. Structura	l characteristics of Ce/Al a	nd (Ce+Al) based samples.
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Campala	SBET	Phase Composition	Dxrd
Sample	(m^2g^{-1})	(Lattice Parameters)	(nm)
Ce/Al	63	$CeO_2(a = b = c = 5.411 \text{ Å})$	40
Ce/Ai	03	$(\theta + \gamma)$ -Al ₂ O ₃	-
2.9 Ea/Ca/A1	50	$CeO_2(a = b = c = 5.411 \text{ Å})$	41
3.8 Fe/Ce/Al		$(\theta + \gamma)$ -Al ₂ O ₃	-
		$CeO_2(a = b = c = 5.411 \text{ Å})$	46
9.9 Fe/Ce/Al	35	$(\theta + \gamma)$ -Al ₂ O ₃	-
		α -Fe ₂ O ₃ (a = b = 5.035 Å, c = 13.741 Å)	32
$(C_0 + \Lambda 1)$	94	$CeO_2(a = b = c = 5.411 \text{ Å})$	11
(Ce + Al)		$(\theta + \gamma)$ -Al ₂ O ₃	tr.
2 E Eo/(Co + A1)	70	$CeO_2(a = b = c = 5.411 \text{ Å})$	12
2.5 Fe/(Ce + Al)		$(\theta + \gamma)$ -Al ₂ O ₃	tr.
		$CeO_2(a = b = c = 5.411 \text{ Å})$	14
6.6 Fe/(Ce + Al)	58	$(\theta + \gamma)$ -Al ₂ O ₃	tr.
		α -Fe ₂ O ₃ (a = b = 5.035Å, c = 13.741 Å)	39

Fe deposition resulted in a decrease in SBET value and a consistent increase in DXRD of CeO₂ species; the value of effect depended on the quantity of Fe (Table 1). Although CeO₂

Catalysts 2022, 12, 938 3 of 16

lattice parameters did not change for all Fe content ranges, the formation of Fe-Ce-O solid solution cannot be excluded. Ceria lattice shrinkage was measured in Au/Ce-Fe-O (Ce/Fe = 9) [17], Fe/CeO₂ (Ce/Fe = 4–9) [18] or CeO₂–Fe₂O₃ (Ce/Fe = 2.3) [19] samples prepared by procedures favoring homogeneous distribution of Fe and Ce in the samples before their high temperature treatment. It was due to the replacement of Ce⁴⁺ ions in the typical cubic fluorite lattice (radius 0.097–0.101 nm) by Fe³⁺ ions (0.049–0.078 nm, depending on coordination and spin state). However, at smaller Fe content in Fe_xCe_{1-x}O₂ (x ≤ 0.05, or Ce/Fe ≥ 20) even a slight increase in lattice parameter compared with pure CeO₂ was observed [18] and related to partial Ce⁴⁺ reduction to the larger (0.123 nm) Ce³⁺ ion [20]. Although in our case Ce/Fe ratio varies within 1.1–6.2, these differently directed effects could compensate for each other because Fe was supported onto support already calcined at 900 °C diminishing the efficiency of its incorporation into CeO₂ lattice, while incorporation of some Fe cations into the alumina component is possible as well.

Nevertheless, neither relative intensity and dispersion of γ -,0-Al₂O₃ changed (Figure S1, inserts), nor α -Al₂O₃ appeared in both Fe/Ce/Al and Fe/(Ce+Al) samples (Figure S1), unlike Fe/Al₂O₃ samples with reasonably close S_{BET} and Fe content values [4]. Hence, the formation of Fe-Al-O solid solutions in Ce-containing samples is hardly ever possible.

2.2. Catalytic Activity in N2O Decomposition and NH3 Oxidation

The activity of Ce/Al and (Ce + Al) based catalysts expressed in terms of N₂O conversion at 800 °C versus Fe content (Figure 1A) is typical for temperature range 700–900 °C (Figure S2). For every type of support, it increases with Fe content. O₂ and H₂O expectedly retard the reaction (Figure S3). Conversion values measured for Fe/(Ce + Al) samples are evidently lower than for Fe/Ce/Al. Therefore, better dispersion of CeO₂ species at close Ce content in the sample does not guarantee higher activity even at higher SBET values (Table 1).

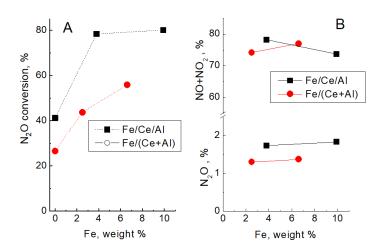


Figure 1. Dependence of N₂O conversion (**A**) and (NO + NO₂) and N₂O yield at NH₃ oxidation (**B**) on Fe content at $800~^{\circ}$ C for Ce/Al and (Ce + Al) based samples.

For all samples, the conversion of NH₃ and yield of (NO + NO₂) (Y_{NO+NO2}) increase, while that of N₂O (Y_{N2O}) decreases with temperature; Y_{NO+NO2} = 74–80% and Y_{N2O} = 0.5–1.8% at T \geq 800 °C (Figures S4 A, B, 1B). High stability for 8 h of operation, at least, was shown as well (Figure S4 C). We estimated that at an NH₃ slip of 1% (although such a value is practically impossible) the increment of N₂O concentration after the Fe-Ce-Al catalyst at 800 °C will be 65–90 ppm. At the average N₂O concentration downstream of the fresh gauzes of 1500 ppm [2], such an addition will diminish N₂O conversion only by 4–6%.

Catalysts 2022, 12, 938 4 of 16

2.3. Microstructure and Morphology

2.3.1. DDPA

Detailed analysis of dissolution kinetics of Fe, Ce and Al in different samples has been presented in corresponding section of Supporting Information. Herein, we summarized and discussed the main facts that are important for understanding the composition and spatial distribution of different compounds in Fe/(Ce + Al) and Fe/Ce/Al samples.

Mixed oxides of different compositions dissolving consecutively in either HCl or HF (Figure S6) represent most of the 2.5 Fe/(Ce + Al) sample (Table 2). The most abundant compound is Fe-Ce-Al mixed oxide with Fe0.03Ce0.09Al stoichiometry which (Figure 2A): encapsulates the particles of Fe-Ce mixed oxide (Fe0.02Ce stoichiometry);

is partially screened by more disordered Fe-Ce-Al mixed oxide with higher content of Fe and Ce (Fe_{0.05}Ce_{0.26}Al stoichiometry) and Fe-Al-O compounds dissolving in HCl.

The decreasing Fe/Al ratio in Fe-Al-O compounds points to the formation of mixed oxide with most disordered near-surface layers enriched by Fen+ (Figure S6 B). At the same time, the protocol of Fe supporting includes using of acidic solutions giving rise to the dissolution of some poorly crystallized alumina detected in the initial support (Figure S5 A, Table 2). In this case, the formation of a γ -FeAlO₃-like compound with spinel structure is quite possible after following drying and calcination at T < 400 °C [21]. Since the mutual Fe₂O₃ and Al₂O₃ solubility in such structure decreased prominently with calcination temperature rise, its decomposition could happen in our case as well leading to the formation of highly dispersed FeOx species (0.06 mmol/g) on the surface of Fe-Al mixed oxide with Fe_{0.05}Al stoichiometry. Its quantity (1.3 mmole/g) is reasonably close to that of alumina dissolving in HCl in the initial support (1.15 mmole/g) (Table 2). Calculation showed that identified soluble compounds include all Al and Fe in the sample, while about 0.7 mmol/g of Ce, or 25% of its general content in the sample, represent insoluble oxides (Tables S1 in Supplementary Materials, Table 2) which are, more probably, small sized CeO2 species with unmodified fluorite lattice (Table 1). Their spatial location in the sample is not clear, but encapsulation by Ce-Al mixed oxide preventing Fe incorporation into the lattice is quite reasonable because the same was detected for the particles of Fe-Ce mixed oxide.

Table 2. Stoichiometry/quantity (mmol/g, without account of for O) of compounds dissolved in HCl and HF flows in different samples. Quantities of insoluble Ce compounds were calculated from balance equations.

Sample	ample Ce + Al 2.5 Fe/(Ce + Al)		3.8 Fe/Ce/Al		
	Al/1.15	Fe/0.06	Fe/0.07		
HCl		Fe _{0.05} Al/1.30	Fe _{0.29} Al/0.37		
	Ce _{0.05} Al/0.67	$Fe_{0.05}Ce_{0.26}Al/0.65$	Fe _{0.19} Ce/0.12		
	Ce _{0.05} Al/7.92	$Fe_{0.05}Ce_{0.26}Al/2.62$	Fe/0.03		
HF	Al/0.45	Fe _{0.03} Ce _{0.09} Al/8.14	Fe _{0.08} Ce _{0.2} Al/2.93		
	Ce/0.069	Fe _{0.02} Ce/0.80	Fe _{0.04} Al/7.47		
Insoluble Ce	2.4	0.7	2.0		

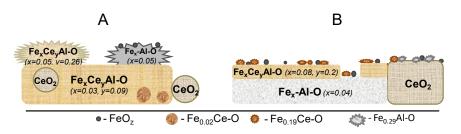


Figure 2. Structures formed in 2.5 Fe/(Ce + Al) (A) and 3.8Fe/Ce/Al (B) samples.

Catalysts 2022, 12, 938 5 of 16

The overall quantity of soluble Ce-containing compounds in the 3.8 Fe/Ce/Al sample is substantially lower as compared with the 2.5 Fe/(Ce + A) sample (Table 2), which can be related to a larger size of CeO₂ particles (Table 1). Most of the dissolved part of the sample is represented by Fe-Al mixed oxide partially screened by Fe-Ce-Al one with Fe_{0.04}Al and Fe_{0.08}Ce_{0.2}Al stoichiometries, correspondingly (Figures S7 C, 2 B, Table 2). Surface layers are composed of more dispersed/disordered binary Fe-Al and Fe-Ce oxides and some FeOx dissolved in HCl (Figure S7, Table 2). Completely independent kinetics of their dissolution can be in the case dispersed FeOx species are located on the surface of any of binary oxides and even non-dissolved large CeO₂ species with unmodified fluorite lattice including 2.0 mmol/g of Ce, or more than 70% of its content in the sample (Figure 2B, Table 2). A substantially higher quantity of Fe in the surface located Fe-Al-O compounds (Fe_{0.29}Al stoichiometry) compared with that in 2.5 Fe/(Ce + Al) could be due to other mechanisms of their formation compared with that in 2.5 Fe/(Ce + Al) sample (see below).

2.3.2. Raman

The band at 462.9 cm⁻¹ in the FT-Raman spectra of Ce/Al sample (Figure 3A) is typical for the F_{2g} vibration mode of the fluorite structure of CeO₂ [22,23]. Its width at ~24.5 cm⁻¹ (Table 3) should correspond to a size of CeO2 species at about 10 nm [23,24] which is substantially less than the estimated value of DxRD at 40 nm (Table 1). At the same time, the particles of 10 nm in a size should be characterized by the Raman band at ~448 cm⁻¹, as follows from experimental dependence obtained for CeO2 and CeO2-Al2O3 composites [15]. Spanier et al. [24] showed that lattice strains in the smaller nanoparticles have the largest contribution to both Raman peak position shift and its broadening compared with other reasons (phonon confinement, particle size distribution, defects, phonon relaxation). Tsunekawa et al. [25] attributed the formation of additional strains to the reduction of Ce4+ ions to Ce³⁺ ions caused by an increasing molar fraction of oxygen vacancies. We supposed that in our case stabilization of additional Ce3+ within fluorite lattice and appearance of strains can be due to insertion of lower sized Al3+ cations into the interstitial sites of c-CeO2 lattice resulting in charge redistribution, such as observed in c-CeO₂/α-Al₂O₃ composites with close Ce/Al ratio [26]. The intensity of the CeO₂ band in the spectra of Fe/Ce/Al samples does not decrease prominently (Table 3), while its position and especially the width become very close to those in the single crystals [23]. Such changes could be due to better ordering of CeO2 structure resulting from Al3+ "extraction" from the lattice after impregnation by acidic Fe-containing solutions that proceed with temperature increase and, to a less extent, some enlargement of crystallized CeO2 species (Table 1). It is the stabilization of small Fe-Al-O clusters in the points of Al insertion into CeO2 lattice after their extraction, but not γ-FeAlO₃ phase decomposing at T > 400 °C, that can be responsible for the substantially higher content of Fe in the Fe-Al mixed oxide (Fe0.29Al) identified by DDPA compared with that in 2.5Fe/(Ce + Al) sample (Table 2). Bands at 231 (not shown), 301, 419 and 622 cm⁻¹ in the spectrum of 9.9 Fe/Ce/Al sample are usually related to lattice vibrations in α -Fe₂O₃ which agrees with XRD data (Table 1).

Catalysts 2022, 12, 938 6 of 16

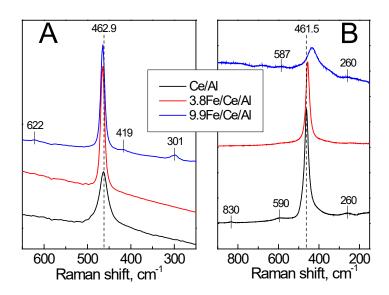


Figure 3. FT-Raman (A) and Raman (B) spectra of Ce/Al-based samples.

Table 3. Position, width (FWHM) and integral intensity of F_{2g} vibrational mode of CeO_2 in the FTRaman and Raman spectra.

Sample	Position, cm ⁻¹		FWHM, cm ⁻¹		Integral Intensity, Arb.Unit	
	FT-Raman	Raman	FT-Raman	Raman	FT-Raman	Raman
Ce/Al	462.9	461.5	24.5	21.2	0.101	30399
3.8 Fe/Ce/Al	465.1	455.8	10.6	21.8	0.087	27805
9.9 Fe/Ce/Al	464.9	433.0	10.8	66.3	0.079	26155
Ce + Al	464.1	462.7	18.3	17.0	0.219	266717
2.5 Fe/(Ce + Al)	464.0	455.8	17.3	23.4	0.0895	34159
6.6 Fe/(Ce + Al)	464.0	459.6	16.3	20.0	0.0327	19715

The absence of the band at ~377 cm⁻¹ related to α -Al₂O₃ phases [27] in the Raman spectra giving information on near subsurface layers of all Ce/Al-based samples (Figure 3B) agrees with XRD and DDPA data. F_{2g} mode of CeO₂ at 461.5 cm⁻¹ in the spectrum of support is supplemented by the bands at ~590, ~260 and ~830 cm⁻¹ ascribed to the vacancyinterstitial (Frenkel-type) oxygen defects, surface mode, and peroxide (O₂²-) stretching vibration at the defective ceria surfaces, respectively [28-30]. These bands disappear in the spectrum of the 3.8Fe/Ce/Al sample because the doping element can annihilate oxygen defects by dopant interstitial compensation mechanism [31]. The low-frequency shift of the CeO2 band and its broadening (Table 3) typical for smaller particles was detected in the spectra of Fe/Ce/Al samples which contradicts the slight increase in averaged sizes of crystalline CeO₂ particles (Table 1). Therefore, the formation of highly dispersed particles of Fe-Ce mixed oxide in the surface layers of the 3.8Fe/Ce/Al samples was detected by DDPA (Table 2) with inhomogeneous strains due to Ce3+ ions therein [15,28] can be responsible for such changes. Asymmetrical broadening with a low-energy shoulder of CeO2 band, especially prominent in the 9.9Fe/Ce/Al sample, can result from a higher concentration of such compounds or higher content of α-Fe₂O₃ therein. In line with this, bands at ~260 and ~590 cm⁻¹ appear again.

The band at 464 cm^{-1} which is responsible for F_{2g} mode of fluorite lattice attenuates drastically in Fe/(Ce + Al) samples compared with that in the initial support (Figure 4A, Table 3). It is, more probably, due to the noticeable additional inclusion of Ce into alumina

Catalysts 2022, 12, 938 7 of 16

or Ce-Al mixed oxides with low Ce content where it exists preferentially as isolated Ce^{3+} ions in the presence of Fe. Indeed, Ce/Al = 0.05 in Ce-Al mixed oxide detected by DDPA in the (Ce + Al) sample but increased up to 0.09-0.26 after Fe supporting (Table 2). The absolute value of mixed oxides increased as well, while the quantity of insoluble CeO_2 decreased from 2.4 mmol/g to 0.7 mmol/g (Table 2). At the same time, the position of CeO_2 F_{2g} mode in Fe/(Ce + Al) samples changed non-substantially pointing to the absence or low degree of ceria lattice modification by foreign atoms compared with the support. In this case, a slightly higher FWHM compared with that in Fe/Ce/Al samples is due to the particle size effect, which is true for crystallized particles, at least (Table 1) [15].

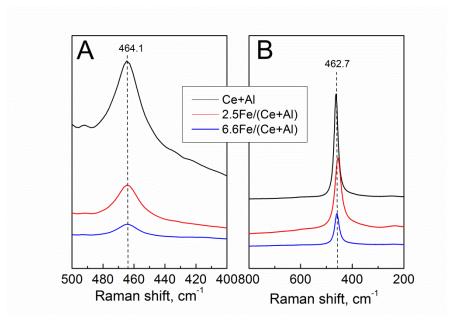


Figure 4. FT-Raman (A) and Raman (B) spectra of (Ce + Al) based samples.

The band at ~377 cm $^{-1}$ related to α -Al₂O₃ phases [27] was absent in the Raman spectra of near subsurface layers of (Ce + Al) based samples as well which agrees with XRD data (Figure S1, Table 1). After iron supporting, they undergo changes that are very similar to those in the bulk of the sample (Figure 4B, Table 3). An even more prominent drop in the intensity of the Ce band compared with that for the bulk can be related to the additional formation of Fe-Ce-Al mixed oxide with high Ce content (Fe0.05Ce0.26Al stoichiometry) (Table 2). Nevertheless, the close CeO₂ band position and FWHM values in FT-Raman and Raman spectra point to a more uniform distribution of elements in the bulk and surface layers of these samples as compared to those in Ce/Al-based samples. This agrees with DDPA data on the preferential formation of Fe-Ce-Al-O mixed oxides in the 2.5 Fe/(Ce + Al) sample, while obviously spatially divided Fe-Al-O, Fe-Ce-O and more CeO₂ were found in the 3.8 Fe/Ce/Al sample.

2.4. Surface Composition (XPS)

The normal complex formed due to shake-down satellites from an O1s to Ce 4f electron transfer in the Ce 3d spectra of all CeO₂ containing samples (Figure 5A) was supplemented by the features marked as v' and u' due to the presence of Ce³⁺ [10]. An increase in Ce³⁺ fraction from 8% of total surface Ce concentration in CeO₂ (spectrum not shown for shortness) up to 20% in 0.86 Fe/CeO₂ sample was related to the formation of Fe-Ce–O solid solution or Fe-Ce mixed oxide [4,32]. Similar compounds of Fe_{0.19}Ce stoichiometry have been detected in the 3.8Fe/Ce/Al sample (Table 2, Figure 2). Therefore, there are two reasons that explain the further increase in Ce³⁺ fraction in 3.8Fe/Ce/Al (25%) and especially Fe/(Ce + Al) (31-33%) samples (Table 4): stabilization of both isolated Ce cations in

Catalysts 2022, 12, 938 8 of 16

alumina-based structure of Fe-Ce-Al mixed oxides (Table 2) and Ce located on CeOx-AlOx boundary in the same oxides as Ce^{3+} ; lower CeO_2 particle sizes (12 nm (2.5 Fe/(Ce + Al)) and 41 nm (3.8 Fe/Ce/Al), Table 1) compared with that in Fe/CeO₂ (55 nm [4]) favoring reduction in Ce^{4+} [25].

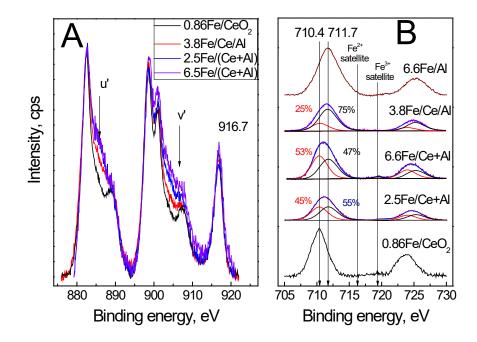


Figure 5. Ce 3d (**A**) Fe 2p (**B**) spectra of Fe-Ce-Al-O samples including contributions of Fe₂O₃ (710.4 eV) and FeOOH (711.7 eV)-like structures to overall Fe₂p spectrum. 6.6 Fe/Al₂O₃ and 0.86 Fe/CeO₂ samples were studied by Pinaeva et al. [4].

Table 4. Surface (XPS) composition of different Fe-Ce-Al-O samples.

Sample	Ce³+, % of Total	Ces, a at. %	Ce _{exp} , rel.units ^b	Ce/Al	Fes ^a at. % ^a	Fe _{exp} , rel.units ^b
3.8 Fe/Ce/Al	25	3.7	184	0.12	1.6	80
2.5 Fe/(Ce + Al)	31	2.4	171	0.075	1.7	117
6.6 Fe/(Ce + Al)	33	2.7	159	0.096	2.7	166

a: calculated supposing C-containing compounds are absent under reaction conditions; accounting of C does not change the order of values. b: calculated as $Fe(Ce)_{exp} = Fe(Ce)_{s}$ -SSA.

Surface Ce concentration (Ces) and Ce/Al ratios in all samples (Table 4) are substantially lower than should follow from its integral composition (Ce/Al \approx 0.3, Table S1), which agrees in general with higher dispersion of Al-containing compounds. The highest Ces and Ce/Al values were measured in the 3.8 Fe/Ce/Al sample (Table 2). However, the concentration of exposed Ce (Ceexp) in the Fe/Ce/Al and Fe/(Ce + Al) samples differ not so prominently because of higher Sbet values in the last (Table 1). It is problematic to estimate Ces in the Fe-Ce-Al-O compounds of the samples. This value should be slightly higher in 2.5Fe/(Ce + Al) sample (Ce/Al = 0.26 instead of Ce/Al = 0.2 for 3.8Fe/Ce/Al sample, Table 2). Surface areas of crystallized CeO2 particles in Fe/(Ce + Al) and Fe/Ce/Al samples as formally estimated from their absolute content (Table S1) and sizes (Table 1) are quite close. However, encapsulation of about 29% of Ce composing Fe-Ce-O mixed oxides (Fe/Ce = 0.02, 0.8 mmol/g, Table 2) by Fe-Ce-Al mixed oxide was found for 2.5 Fe/(Ce + Al) sample (Figure 2A). This allows supposing bulk location of some CeO2 species as well thus decreasing Ces value therein. In addition, preferential exposing of highly dispersed

Catalysts 2022, 12, 938 9 of 16

Fe-Ce-O compound with Fe_{0.19}Ce stoichiometry can additionally contribute to higher Ce_s value in the 3.8 Fe/Ce/Al sample. Hence, a substantial part of Ce_s in the Fe/(Ce + Al) samples composes Fe-Ce-Al mixed oxides with a high concentration of Ce⁺, while the fraction of CeO₂-like structures is higher and seems to be responsible for greater Ce_s value in Fe/Ce/Al samples.

The 3.8 Fe/Ce/Al sample is characterized by the lowest Fe surface concentration (Fe_s) and the quantity of exposed Fe as related to a weight unit (Feexp) (Table 4). BE values of the Fe2p3/2 spectra ranging from 710.9 eV to 711.7 eV (Figure 5B) evidence presence of Fe³⁺in oxyhydroxide environment (like in α - or γ -FeOOH), and in the oxide (like Fe₂O₃) structures [33–35], correspondingly dominating in 6.6 Fe/Al₂O₃ and 0.86 Fe/CeO₂ samples [4]. Although the positions of the Fe 2P_{3/2} peak for Fe²⁺ in Fe_{0.94}O, 2FeO·SiO₂ or Fe_{0.01}Mg_{0.99}O(100) single crystal were characterized by the values between 709.0 and 710.4 eV, its absence or low content in our samples follows from the absence of distinct satellite at 714.6–716 eV [36,37]. FeOOH usually undergoes a dehydroxylation reaction at 250–300 °C resulting in Fe₂O₃ [38]. At the same time, tetrahedral Fe³⁺ cations coordinating both terminal and bridging OH groups were found on the surface of both Fe-Al-O solid solution and highly dispersed FeOx species resulting from the decomposition of γ-FeAlO₃-like structures [21]. In accordance with this, the Fe2p_{3/2} band at 711.7 eV (dominates in 3.8Fe/Ce/Al sample) can be subscribed to: Fe³⁺ ions in Fe-Al mixed oxides, including those with Fe0.29Al stoichiometry (Table 2) formed by "extraction" of Al from CeO2 lattice after Fe supporting; highly dispersed FeOx species resulted from the decomposition of Fe-Al-O.

The band at 710.4 eV can characterize FeOx species on the surface of CeO_2 or Fe^{3+} ions in the Fe-Ce-O compounds (Table 2, Figure 2). Its high abundance in Fe/(Ce + Al) samples (45–53% of total Fe $_8$) contradicts lower Ce $_8$ values compared with that in 3.8 Fe/Ce/Al sample. However, the substantial part of the surface Fe in Fe/(Ce + Al) samples composes Fe-Ce-Al mixed oxides with reasonably high Ce content (Ce/Al = 0.26, Table 2). It resulted from the inclusion of additional Ce from CeO $_2$ into the surface layers of alumina or Ce-Al mixed oxide of the initial support with Fe participation. Therefore, preferential formation of Fe-Ce-O oxide-like compounds is quite possible in Fe-Ce-Al mixed oxides. The contribution of Fe-Ce-Al mixed oxides into the surface composition in the 3.8 Fe/Ce/Al sample is not high which follows from the preferential dissolution of FeOx, binary Fe-Al-O and Fe-Ce-O compounds in HCl (Table 2) and substantially less prominent decrease in integral intensity of F $_{2g}$ vibrational mode of CeO $_2$ in the near-surface layers of Fe/Ce/Al samples compared with corresponding support (Table 3).

2.5. O₂ Adsorption/Desorption

 O_2 transients recorded during the He/0.5vol.% O_2 switch following 60 s stay in He flow revealed the delay of O_2 response compared with Ar (Figure 6) corresponding to adsorption of reasonably close quantities of oxygen (3 × 10^{19} –5 × 10^{19} oxygen atom/g) by reduced sites in the 2.5 Fe/(Ce + Al) and 3.8 Fe/Ce/Al samples.

Catalysts 2022, 12, 938 10 of 16

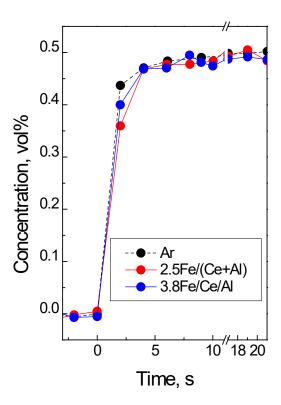


Figure 6. Responses of O_2 and inert label (Ar) during the switch from He to He + 0.5vol.% O_2 flow over different samples. T = 800 $^{\circ}$ C.

Differently paired Fe²⁺ and Ce³⁺ ions resulting from the reduction in the oxygen absence are the most evident sites for O₂ dissociative adsorption as coordinatively unsaturated surface metal cations. They can form in the surface layers of FeO_x clusters, including those resulted from the decomposition of α -FeAlO₃; Fe-Al-O mixed oxide of Fe_{0.29}Al stoichiometry formed in 3.8Fe/Ce/Al sample by Al "extraction" from CeO₂ lattice during calcination; highly dispersed Fe-Ce mixed oxides (Fe_{0.19}Ce stoichiometry (Table 2); Fe-Al-Ce-O mixed oxides with high Ce content (Fe_{0.05}Ce_{0.26}Al or Fe_{0.08}Ce_{0.2}Al stoichiometry).

Reduction of isolated Fe³⁺ in the Fe-Al-(Ce-)O mixed oxides with of Fe_{0.03}Ce_{0.09}Al stoichiometry (most of Ce stabilized as Ce³⁺ and unlikely can participate in any redox processes) requires transport of second oxygen atom through the occasional vacancies on the surface or in the bulk of alumina and thus be slow.

2.6. Oxygen Mobility (18O SSITKA)

The rates of oxygen exchange in Fe/Ce-Al-O samples in the period of 0–60 s after the $^{16}\text{O}/^{18}\text{O}$ switch can be ordered as 3.8 Fe/Ce/Al > 6.6 Fe/(Ce + Al)>2.5 Fe/(Ce + Al), as follows from the slope of No(t)/g dependencies (Figure 7A). It does not correlate with Sbet values of the samples (Table 1) and Fes or Feexp values (Table 4). Moreover, the difference between 3.8 Fe/Ce/Al and Fe/(Ce + Al) samples becomes even more prominent when related to one surface Fe site (Figure 7B). Fast exchange proceeding with reasonably close to initial rate value in these samples during about 20-25 s includes a higher quantity of oxygen atoms (No = $1 \times 10^{21} - 2 \times 10^{21}$ O atoms/g) than can be related to Fe, even with an account of that located in the bulk ($\sim 1.0 \times 10^{21}$ O atoms/g in the 6.6 Fe/(Ce + Al) sample with the highest Fe content). Therefore, efficient exchange in the near-surface layers of Ce-containing compounds contributes to No as well. Indeed, substantially more profound and faster oxygen exchange took place in Fe/CeO₂ samples compared with Fe/Al₂O₃ [4]. However, both Ce

Catalysts 2022, 12, 938 11 of 16

content and Ce_{exp} values are reasonably close in all samples (Table 4). We consider that the higher rate of exchange in the 3.8 Fe/Ce/Al sample can be due to preferential exposure of Fe-Ce mixed oxide or crystallized CeO₂, including that bonded with clusters of FeOx or Fe-Al mixed oxides, while in 2.5 Fe/(Ce + Al) sample substantial part of Fe and Ce are included as preferentially isolated ions into Fe-Ce-Al mixed oxides that still retain alumina-like structure. Although Fe-Ce mixed oxide was detected in the 2.5 Fe/(Ce + Al) sample (Table 2, Figure S6), it obviously locates in bulk (Figure 2), like part of CeO₂, and thus does not contribute to the fast oxygen exchange.

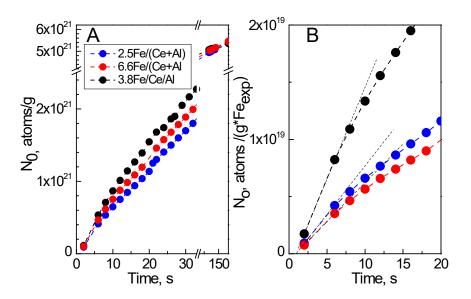


Figure 7. Time dependencies of the quantity of exchanged oxygen (No) as related to weight unit (A) or one surface Fe site (B) in 18 O SSITKA experiments for different samples. T = $800 \, ^{\circ}$ C.

2.7. Discussion

In accordance with the simplified redox scheme of N_2O decomposition proposed by Kapteijn et al. [39]:

$$N_2O + * \rightarrow N_2 + O*$$

 $2O^* \mapsto 2^* + O_2$

one active (reduced) site is sufficient for N_2 to evolve, but two neighboring O* are necessary for the desorption of O_2 . Factually, two neighboring active sites for N_2O adsorption are desired for efficient reaction running, especially provided oxygen desorption from the surface is the rate-controlling step of this reaction [39]. Potential quantities of such reduced sites under reaction conditions in 2.5 Fe/(Ce + Al) and 3.8 Fe/Ce/Al samples are quite close (Figure 6). At the same time, the isotopic transient experiment $^{18}O_2/N_2^{16}O$ performed on LaMnO₃ at 900 °C revealed that there is direct oxygen transfer to the catalysts' bulk from N_2O molecule, and O_2 formed involves lattice oxygen [40]:

$$2N_2{}^{16}O + 2{}^{18}O_{latt} \ \rightarrow {}^{18}O_2 + 2{}^{16}O_{latt} + 2N_2$$

This means that catalytic activity should depend on oxygen exchange properties.

In CeO₂-containing compounds a simplified redox scheme realized in Fe oxides or FeOx/Al₂O₃ systems:

1A)
$$Fe^{2+} + N_2O \rightarrow N_2 + Fe^{3+}O$$

is supplemented by analogous steps for Ce³⁺/Ce⁴⁺ redox pair:

1B)
$$Ce^{3+} + N_2O \rightarrow N_2 + Ce^4-O$$

Catalysts 2022, 12, 938 12 of 16

And step corresponding to the additional pathway of oxygen species recombination provided by the presence of neighboring Fe³⁺and Ce⁴⁺:

2C)
$$Fe^{3+}O + Ce^{4+}O \rightarrow Fe^{2+} + Ce^{3+} + O_2$$

In addition, reoxidation of Ce³⁺ due to fast oxygen diffusion from CeO₂ lattice (O_{lat}) by extended oxygen vacancies arising after insertion of Fe³⁺ ions into the fluorite lattice:

3)
$$O_{lat} + Ce^{3+} \longrightarrow Ce^{4+}O$$

Can become an alternative pathway for the supply of the second oxygen atom which is necessary for O₂ desorption and enhancing recombination of oxygen adspecies by steps 2B and 2C without adsorption of the second N₂O molecule. Pure CeO₂ revealed insubstantial activity as related per surface area unit compared with FeO_x/CeO₂ and even Fe/Al₂O₃ samples [4]. Therefore, the contribution of this pathway is high in Fe/Ce/Al samples containing substantial quantities of both Fe-Ce-O mixed oxide and bulky CeO₂ bonded with FeO_x or Fe-Al-O clusters. Stabilization of a substantial fraction of Ce as isolated Ce³⁺ cations composing mixed Fe-Ce-Al oxides in the Fe/(Ce + Al) samples diminishes substantially the efficiency of oxygen transfer to Fe³-O sites.

3. Materials and Methods

3.1. Catalysts Preparation

Two procedures were used to prepare the supports with a CeO₂ : Al₂O₃ weight ratio of 1 : 1. In the first of them, the precursor of CeO₂ was deposited from 0.75 M Ce(NO₃)₃·6H₂O (99.0%, Vekton, Saint-Petersburg, Russia) water solution using 1 M (NH₄)₂CO₃ (99.3 %, Vekton, Saint-Petersburg, Russia) as a precipitation agent onto Al₂O₃ (the product of thermochemical activation of hydrargillite calcined at 500 °C) characterized by BET surface area at 210 m²g⁻¹). After washing by H₂O unless the pH of the filtrate was 7 and drying at 60°C overnight, the sample was calcined at 900 °C for 5 h and denoted below as Ce/Al. In the second procedure, the water solution of (NH₄)₂CO₃ was added dropwise to a water solution of Al(NO₃)₃·9H₂O (98.5%, Ecros, Saint-Petersburg, Russia) and Ce(NO₃)₃·6H₂O mixed in the necessary proportion unless (Ce + Al)/CO₃ (mole) = 2.5 value was reached. Thus, the obtained gel was dried at 60 °C for 22 h followed by calcination at 500 °C for 2h and at 900 °C for 5h resulting in a sample denoted below as (Ce + Al).

FeO_x was supported by incipient wetness impregnation of Ce/Al and (Ce + Al) by water solution of Fe(NO₃)₃·9H₂O (98.5 %, Vekton, Saint-Petersburg, Russia) with necessary concentration with added citric acid (99.8 %, Vekton, Saint-Petersburg, Russia) in 10 wt.% excess to the stoichiometric amount and ethyleneglycole (99.0 %, Ecros, Saint-Petersburg, Russia), dried in air at 150 °C for 3 h and then calcined at 900 °C for 4 h. In the commonly used abbreviation n Fe/support, "n" corresponded to Fe weight % concentration in the sample.

3.2. Characterization

XRD patterns were recorded using D8 diffractometer (Bruker, Germany) with CuK α monochromatic radiation. Each sample was scanned in the range of 2θ from 10° to 70° with a step 0.05° . The surface composition of the samples was investigated by X-ray photoelectron spectroscopy (XPS) using spectrometer SPECS (SPECS, Germany) with Al K α irradiation (hv = 1486.6 eV). The positions of the peaks of Au $4f_{7/2}$ (84.0 eV) and Cu $2p_{3/2}$ (932.67 eV) core levels were used for calibration of the binding energy (BE) scale. In Raman spectroscopy depth of light penetration depends on the wavelength of monochromatic radiation provided by different sources. We believe that green light (514.5 nm line of an Ar⁺ laser with 2 mW power reaching the sample) provides information about the structure of preferentially near-surface layers of the samples, while data on the bulk composition are obtained with near-infrared (NIR) radiation at 1064 nm line (provided by an Nd-YAG laser with 100 mW power output) (Bruker Optik GmbH, Ettlingen, Germany). FT-Raman spectra (3700–100 cm⁻¹, 300 scans, resolution 4 cm⁻¹, 180° geometry) were collected using an RFS 100/S spectrometer (Bruker Optik GmbH, Ettlingen, Germany). Horiba Jobin Yvon

Catalysts 2022, 12, 938 13 of 16

T64000 spectrometer (HORIBA Scientific, Palaiseau, France) with micro-Raman setup and backscattering geometry for experimental spectra collection was used to measure the Raman spectra. The spectral resolution was not worse than 1.5 cm⁻¹. The detector was a silicon-based CCD matrix, cooled with liquid nitrogen. The band at 520.5 cm⁻¹ of Si single crystal was used to calibrate the spectrometer.

The method of differential dissolution phase analysis (DDPA) [41] was used to reveal the composition and, in some cases, morphology and particle depth distribution of the compounds and phases (including X-Ray amorphous ones) formed in the samples. For this about 10 mg of the sample loaded in a quartz microreactor was dissolved in the flow (3.6 mL/min) of water-based solution with the composition changing from HCl (pH = 2) to 3M HCl (with continuous temperature increase from 20 °C to 90 °C), and finally to 3.6 M HF. Compounds dissolving in milder conditions (HCl (pH = 2) and 1–3M HCl) were reasonably supposed to form in the surface layers of the samples. Better crystallized structures, as a rule, dissolve in HF or even remain insoluble. Change of the outlet mixture composition in time was analyzed by ICP AES 262477-364A spectrometer (BAIRD, Zoeterwoude, The Netherlands) using the spectral lines at 238.2, 308.2, and 413.8 nm which are characteristic for Fe, Al and Ce, respectively.

3.3. Kinetic Measurements and Catalytic Tests

For ¹⁶O/¹⁸O exchange experiments, the sample was first heated to 800 °C in 0.58 vol %16O₂ + He flow and kept at this temperature for 30 min. After, this gas mixture was replaced stepwise by the same one containing ¹⁸O₂ and Ar (1 vol.%) as an inert tracer. All responses were analyzed using QMS 200 gas analyzer (Stanford Research Systems, Sunnyvale, USA) as time variation of the ¹⁸O atomic fraction in the gas phase $\alpha_g(t)$ = $\frac{(0.012*0.030)}{2*(160^{18}0+180^{18}0+160^{16}0)}$. Time dependencies of exchanged oxygen for different samples as $(^{16}0^{18}0 + 2*^{18}0^{18}0)$ related to the mass unit (No) were calculated using the formulae $N_0(t) = N_A * \frac{2*C_{02}*U}{g} *$ $\int_0^t (\alpha_g^{input} - \alpha_g) dt$, where α_g^{input} : isotope fraction in the inlet mixture (0.95), Co₂: inlet O₂ concentration (mol/mol), U: flow rate of the reaction mixture (mole/s), NA: Avogadro number. Dynamics of oxygen adsorption/desorption at 800 °C was elucidated from the experiments on the stepwise replacement of He by 0.5 vol.%O₂ + 1 vol.%Ar + He mixture and vice versa flowing the reactor. (O₂ + He)/He switch was performed after at least 30 min sample stay in O₂ containing flow, while He/(O₂ + He) one followed in about 60 s. All kinetic measurements were performed with the sample (g = 0.025 g, particles of 250–500 μm in a size) loaded into a reactor (quartz tube, i.d. = 3 mm). The gas flow rates of all mixtures amounted to 16.7 cm³/s.

The catalytic activity for samples with particles of 250–500 μm in a size was measured in a fixed-bed U-shaped reactor (3 mm i.d. quartz tube) at ambient pressure in the temperature range 700–900 °C. For NH³ oxidation, mixture 1% NH³ + 20% O² in N² was fed to the reactor charged by 0.015 g of the sample with a flow rate of 6.9 cm³/s. Concentrations of NH³ and NOx (x = 0.5-2) in the outlet mixture were measured by infrared spectroscopy. For N²O decomposition, a gas mixture of 0.15 vol% N²O in He flowed the reactor charged with 0.038 g of the sample with a flow rate of 16.7 cm³/s. In some experiments about 3 vol.% O² (+3 vol.% H²O) were added to the inlet mixture. Outlet mixture composition was analyzed by gas chromatograph equipped with Porapack T (i.d. = 3mm, l = 3 m, for N²O analysis) and NaX (i.d. = 3mm, l = 2 m, for N² analysis) columns. N²O or NH³ conversion (XN²O(NH³)) and yield (Y¹) values calculated as $X_{N2O} = \frac{(C_{N2O}^0 - C_{N2O})}{C_{N2O}^0} * 100\%$, $X_{NH3} = \frac{(C_{NH3}^0 - C_{NH3})}{C_{NH3}^0} * 100\%$, and $Y_i = \frac{n*C_i}{C_{NH3}^0} * 100\%$, (C₁ and C₁°: outlet and inlet concentrations of *i*th compound, n: number of N atoms in the *i*th molecule) were considered as a measure of samples activity.

Catalysts 2022, 12, 938 14 of 16

4. Conclusions

FeOx (2.5–9.9 weight.% in terms of Fe) was supported by impregnation of mixed CeO_2 -Al₂O₃ support prepared either by co-precipitation (Ce + Al) or CeO₂ precipitation onto Al₂O₃ (Ce/Al). Preferentially Fe-Ce-Al mixed oxides both in the surface layers and in the bulk were formed in Fe/(Ce + Al) samples, while the substantial spatial division of ceria and alumina-based compounds remains intact in Fe/Ce/Al samples. The stabilization of Ce^{3+} in Fe-Ce-Al mixed oxides was shown to inhibit oxygen mobility in the near-surface layers of Fe/(Ce + Al) samples. It results in retardation of the additional pathway of oxygen supply to the sites responsible for O₂ desorption and explains the lower activity of Fe/(Ce + Al) samples in N₂O decomposition.

Supplementary Materials: The following supporting information can be downloaded at: https://www.mdpi.com/article/10.3390/catal12090938/s1, Figure S1: XRD patterns of Ce/Al (A) and (Ce + Al) (B) based samples with different content of Fe, Figure S2: Dependence of N2O conversion on the temperature for Ce/Al (A) and (Ce + Al) (B) based samples, Figure S3: Effect of O2 and H2O presence in the inlet flow on N_2O conversion over 3.8 Fe/Ce/Al and 2.5 Fe/(Ce + Al) samples. T = 800 ^oC, Figure S4: Temperature dependence of the conversion (A) yield of (NO + NO₂) and N2O (B) at NH₃ oxidation over different Fe/Ce-Al-O based samples. Stability tests for 9.9 Fe/Ce/Al sample (C) at 800 °C, Figure S5: Differential dissolution curves of Ce and Al (A) and identified compounds (B) at stepwise consecutive change of flow composition from HCl (pH = 2) to 1-3M HCl (1) and then to 3.6 M HF (2) over (Ce + Al) sample, Figure S6: Differential dissolution curves of Fe, Ce and Al (A) and identified compounds (B) at stepwise consecutive change of flow composition from HCl (pH = 2) to 1-3M HCl (1) and then to 3.6 M HF (2) over 2.5 Fe/(Ce + Al) sample, Figure S7: Differential dissolution curves of Fe, Ce and Al (A) and initially (B) and finally (C) identified Fe-Ce-Al compounds at stepwise consecutive change of flow composition from HCl (pH = 2) to 1–3M HCl (1) and then to 3.6 M HF (2) over 3.8Fe/Ce/Al sample; Table S1: Quantity of Fe, Ce, Al (as prepared, dissolved and insoluble) in different samples (mmol/g). Quantities of insoluble compounds were calculated from balance equations.

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References

- 1. Groves, M.C.E.; Sasonow, A. Uhde EnviNOx® technology for NOx and N2O abatement: A contribution to reducing emissions from nitric acid plants. *J. Integr. Environ. Sci.* **2010**, *7*, 211–222.
- 2. Pérez-Ramírez, J.; Kapteijn, F.; Schöffel, K.; Moulijn, J.A. Formation and control of N₂O in nitric acid production. Where do we stand today? *Appl. Catal. B Environ.* **2003**, 44, 117–151.
- 3. Sadykov, V.A.; Isupova, L.A.; Zolotarskii, I.A.; Bobrova, L.N.; Noskov, A.S.; Parmon, V.N.; Brushtein, E.A.; Telyatnikova, T.V.; Chernyshev, V.I.; Lunin, V.V. Oxide catalysts for ammonia oxidation in nitric acid production: Properties and perspectives. *Appl. Catal. A Chem.* **2000**, 204, 59–87.
- 4. Pinaeva, L.G.; Prosvirin, I.P.; Dovlitova, L.S.; Danilova, I.G.; Sadovskaya, E.M.; Isupova, L.A. MeOx/Al2O3 and MeOx/CeO2 (Me = Fe, Co, Ni) catalysts for high temperature N2O decomposition and NH3 oxidation. *Catal. Sci. Technol.* **2016**, *6*, 2150–2161.
- 5. Pinaeva, L.G.; Dovlitova, L.S.; Isupova, L.A. Monolithic FeOx/Al₂O₃ Catalysts for Ammonia Oxidation and Nitrous Oxide Decomposition. *Kinet. Catal.* **2017**, *58*, 167–178.
- 6. Giecko, G.; Borowiecki, T.; Gac, W.; Kruk, J. Fe₂O₃/Al₂O₃ catalysts for the N₂O decomposition in the nitric acid industry. *Catal. Today* **2008**, 137, 403–409.
- 7. Kruk, J.; Stołecki, K.; Michalska, K.; Konkol, M.; Kowalik, P. The influence of modifiers on the activity of Fe₂O₃ catalyst for high temperature N₂O decomposition (HT-deN₂O). *Catal. Today* **2012**, *191*, 125–128.

Catalysts 2022, 12, 938 15 of 16

8. Sádovská, G.; Tabor, E.; Bernauer, M.; Sazama, P.; Fíla, V.; Kmječ, T.; Kohout, J.; Závěta, K.; Tokarová, V.; Sobalík, Z. FeOx/Al₂O₃ catalysts for high-temperature decomposition of N₂O under conditions of NH₃ oxidation in nitric acid production. *Catal. Sci. Technol.* **2018**, *8*, 2841–2852.

- 9. Imagawa, H.; Suda, A.; Yamamura, K.; Sun, S. Monodisperse CeO₂ Nanoparticles and Their Oxygen Storage and Release Properties. *J. Phys. Chem.* C **2011**, *115*, 1740–1745.
- 10. Chen, L.; Fleming, P.; Morris, V.; Holmes, J.D.; Morris, M.A. Size-Related Lattice Parameter Changes and Surface Defects in Ceria Nanocrystals. *J. Phys. Chem.* C **2010**, *114*, 12909–12919.
- 11. Iwanek, E.; Krawczyk, K.; Petryk, J.; Sobczak, J.W.; Kaszkur, Z. Direct nitrous oxide decomposition with CoOx-CeO₂ catalysts. *Appl. Catal. B Environ.* **2011**, *106*, 416–422.
- 12. Grzybek, G.; Stelmachowski, P.; Gudyka, S.; Indyka, P.; Sojka, Z.; Guillén-Hurtado, N.; Rico-Pérez, V.; Bueno-López, A.; Kotarba, A. Strong dispersion effect of cobalt spinel active phase spread over ceria for catalytic N₂O decomposition: The role of the interface periphery. *Appl. Catal. B Environ.* **2016**, *180*, 622–629.
- 13. Ferreira, A.P.; Zanchet, D.; Rinaldi, R.; Schuchardt, U.; Damyanova, S.; Bueno, J.M.C. Effect of the CeO₂ content on the surface and structural properties of CeO₂–Al₂O₃ mixed oxides prepared by sol–gel method. *Appl. Catal. A Chem.* **2010**, *388*, 45–56.
- 14. Damyanova, S.; Perez, C.A.; Schmal, M.; Bueno, J.M.C. Characterization of ceria-coated alumina carrier. *Appl. Catal. A Chem.* **2002**, 234, 271–282.
- 15. Boullosa-Eiras, S.; Vanhaecke, E.; Zhao, T.; Chen, D.; Holmen, A. Raman spectroscopy and X-ray diffraction study of the phase transformation of ZrO₂–Al₂O₃ and CeO₂–Al₂O₃ nanocomposites. *Catal. Today* **2011**, *166*, 10–17.
- 16. Ge, C.; Liu, L.; Liu, Z.; Yao, X.; Cao, Y.; Tang, C.; Gao, F.; Dong, L. Improving the dispersion of CeO₂ on γ-Al₂O₃ to enhance the catalytic performances of CuO/CeO₂/γ-Al₂O₃ catalysts for NO removal by CO. *Catal. Commun.* **2014**, *51*, 95–99.
- 17. Laguna, O.H.; Romero Sarria, F.; Centeno, M.A.; Odriozola, J.A. Gold supported on metal-doped ceria catalysts (M = Zr, Zn and Fe) for the preferential oxidation of CO (PROX). *J. Catal.* **2010**, *276*, 360–370.
- 18. Zhang, Z.; Han, D.; Wei, S.; Zhang, Y.; Determination of active site densities and mechanisms for soot combustion with O₂ on Fe-doped CeO₂ mixed oxides. *J. Catal.* **2010**, 276, 16–23.
- 19. Li, K.; Wang, H.; Wei, Y.; Yan, D. Direct conversion of methane to synthesis gas using lattice oxygen of CeO₂–Fe₂O₃ complex oxides. *Chem. Eng. J.* **2010**, *156*, 512–518.
- 20. Gupta, A.; Kumar, A.; Waghmare, U.V.; Hegde, M.S.; Origin of activation of Lattice Oxygen and Synergistic Interaction in Bimetal-Ionic Ceo.89Feo.1Pdo.01O2-6 Catalyst. *Chem. Mater.* **2009**, *21*, 4880–4891.
- 21. Escribano, V.S.; Amores, J.M.G.; Finocchio, E.; Daturi, M.; Busca, G. Characterization of α-(Fe,Al)₂O₃ solid-solution powders. *J. Mater. Chem.* **1995**, *5*, 1943–1951.
- 22. McBride, J.R.; Hass, K.C.; Poindexter, B.D.; Weber, W.H. Raman and x-ray studies of Ce_{1-x}RExO_{2-y} where RE=La, Pr, Nd, Eu, Gd, and Tb. *J. Appl. Phys.* **1994**, *76*, 2435–2441.
- 23. Kosacki, I.; Suzuki, T.; Anderson, H.U.; Colomban, P. Raman scattering and lattice defects in nanocrystalline CeO₂ thin films. *Solid State Ion.* **2002**, 149, 99–105.
- 24. Spanier, J.E.; Robinson, R.D.; Zhang, F.; Chan, S.W.; Herman, I.P. Size-dependent properties of CeO_{2-y} nanoparticles as studied by Raman scattering. *Phys. Rev. B* **2001**, *64*, 245407.
- 25. Tsunekawa, S.; Ishikawa, K.; Li, Z.Q.; Kawazoe, Y.; Kasuya, Y. Origin of Anomalous Lattice Expansion in Oxide Nanoparticles. *Phys. Rev. Lett.* **2000**, *85*, 3440–3443.
- 26. Ojha, A.K.; Ponnilavan, V.; Kannan, S. Structural, morphological and mechanical investigations of in situ synthesized c-CeO₂/α-Al₂O₃ composites. *Ceram. Int.* **2017**, 43, 686–692.
- 27. Porto, S.P.S.; Krishnan, R.S. Raman Effect of Corundum. J. Chem. Phys. 1967, 47, 1009–1012.
- 28. Sudarsanama, P.; Malleshama, B.; Reddy, P.S.; Großmann, D.; Grünert, W.; Reddy, B.M. Nano-Au/CeO₂ catalysts for CO oxidation: Influence of dopants (Fe, La and Zr) on the physicochemical properties and catalytic activity. *Appl. Catal. B Environ.* **2014**, *144*, 900–908.
- 29. Schilling, C.; Hofmann, A.; Hess, C.; Ganduglia-Pirovano, M.V. Raman Spectra of Polycrystalline CeO₂: A Density Functional Theory Study. *J. Phys. Chem. C* **2017**, 121, 20834–20849.
- 30. Reina, T.R.; Ivanova, S.; Centeno, M.A.; Odriozola, J.A. Boosting the activity of a Au/CeO₂/Al₂O₃ catalyst for the WGS reaction. *Catal. Today* **2015**, *253*, 149–154.
- 31. Laguna, O.H.; Centeno, M.A.; Boutonnet, M.; Odriozola, J.A. Fe-doped ceria solids synthesized by the microemulsion method for CO oxidation reactions. *Appl. Catal. B Environ.* **2011**, *106*, 621–629.
- 32. Perez-Alonso, F.J.; Melián-Cabrera, I.; López Granados, M.; Kapteijn, F.; Fierro, J.L.G. Synergy of FexCe_{1-x}O₂ mixed oxides for N₂O decomposition. *J. Catal.* **2006**, 239, 340–346.
- 33. Suzuki, S.; Yanagihara, K.; Hirokawa, K. XPS study of oxides formed on the surface of high-purity iron exposed to air. *Surf. Interface Anal.* **2000**, *30*, 372–376.
- 34. Grosvenor, A.P.; Kobe, B.A.; Biesinger, M.C.; McIntyre, N.S. Investigation of multiplet splitting of Fe 2p XPS spectra and bonding in iron compounds. *Surf. Interface Anal.* **2004**, *36*, 1564–1574.
- 35. Atuchin, V.V.; Vinnik, D.A.; Gavrilova, T.A.; Gudkova, S.A.; Isaenko, L.I.; Jiang, X.; Pokrovsky, L.D.; Prosvirin, I.P.; Mashkovtseva, L.S.; Lin, Z. Flux Crystal Growth and the Electronic Structure of BaFe₁₂O₁₉ Hexaferrite. *J. Phys. Chem. C* **2016**, 120, 5114–5123.
- 36. Yamashita, T.; Hayes, P. Analysis of XPS spectra of Fe²⁺ and Fe³⁺ ions in oxide materials. Appl. Surf. Sci. 2008, 254, 2441–2449.

Catalysts 2022, 12, 938 16 of 16

37. Merte, L.R.; Gustafson, J.; Shipilin, M.; Zhang, C.; Lundgren, E. Redox behavior of iron at the surface of an Feo.01Mg0.99O(100) single crystal studied by ambient-pressure photoelectron spectroscopy. *Catal. Struct. React.* **2017**, *3*, 95–103.

- 38. Sayed, F.N.; Polshettiwar, V. Facile and sustainable synthesis of shaped iron oxide nanoparticles: Effect of iron precursor salts on the shapes of iron oxides. *Sci. Rep.* **2015**, *5*, 09733.
- 39. Kapteijn, F.; Rodriguez-Mirasol, J.; Moulijn, J. Heterogeneous catalytic decomposition of nitrous oxide. *Appl. Catal. B Environ.* **1996**, *9*, 25–64.
- 40. Ivanov, D.V.; Pinaeva, L.G.; Sadovskaya, E.M.; Isupova, L.A. Isotopic transient kinetic study of N2O decomposition on LaMnO3+6. *J. Mol. Catal. A Chem.* **2016**, 412, 34–38.
- 41. Malakhov, V.; Boldyreva, N.; Vlasov, A.; Dovlitova, L. Methodology and procedure of the stoichiographic analysis of solid inorganic substances and materials. *J. Analyt. Chem.* **2011**, *66*, 458–464.